

Study of the post-combustion CO₂ capture applied to conventional and partial oxy-fuel cement plants

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Carbon dioxide emitted from the cement industry represents 30% of the total annual CO₂ released by the industrial sector. Reducing carbon dioxide industrial emissions became one of the most investigated issues nowadays. For this purpose, it is necessary to optimize the application of Carbon Capture and Storage (CCS) or Carbon Capture and re-Use (CCU) to all the major CO₂-emitting industries. The present communication is focusing on the application of CCU to the cement industry, more specifically on the CO₂ capture step.

The objective of this work is to test the applicability to the cement industry of an innovative capture technique called partial oxyfuel combustion capture. This technology combines a O₂-enriched air combustion involving a CO₂ more concentrated flue gas (20 % < y_{CO₂} < 70 %) compared to a conventional combustion and allowing the application of a CO₂ post-combustion capture using amine solvents. Indeed, thanks to a more CO₂-concentrated flue gas and the choice of an adequate solvent, this process assures a decrease of the regeneration energy [1-3] in the amine plant (compared to the conventional post-combustion) as well as reducing the cost of O₂ production (O₂-enriched air) in the Air Separation Unit (ASU) compared to total oxyfuel conditions (pure O₂).

In our first studies, the performances of several solvents were evaluated thanks to continuous tests carried out at lab scale (cables-bundle contactor) considering high CO₂ contents (y_{CO₂,in} = 20-60 vol.%). Simple and activated solvents were screened in such conditions and compared: primary alkanolamines (Monoethanolamine (MEA)), secondary alkanolamines (Diethanolamine (DEA) and Methylmonoethanolamine (MMEA)), tertiary alkanolamines (N-methyldiethanolamine (MDEA)), sterically hindered amines (2-amino-2-methyl-1-propanol (AMP) and 2-amino-2-hydroxymethyl-1,3-propanediol (AHPD)), cyclical diamines (Piperazine (PZ)) and non-cyclical tetramines (Triethylenetetramine (TETRA)). Based on the results obtained at lab scale [4], semi-continuous tests at micro-pilot scale (Fig. 1) were conducted for the best solvents screened and results were confirmed (Fig. 2): for the simple solvents, the system MMEA 30% presents the best absorption performances and the use of the activated solutions of AMP or DEA with PZ 5 wt.% leads particularly to high absorption performances both in conventional and high CO₂ contents conditions, the performances becoming even better than conventional solvents such as MEA 30 wt.% (all values are taken once the regime phase of the test is achieved). Simulation tests of the micro-pilot unit using Aspen Hysys software V8.8 for MEA 30% and experimental results (Fig. 3) for all the solvents showed that **the regeneration energy decreases when increasing the CO₂ content in the gas to treat.**

As a prospect, further works will present for the most performant solvents, a complete and optimized study including both the energy costs associated to the O₂ production (ASU) for the partial oxy-fuel conditions and the costs (OPEX and CAPEX) of the post-combustion CO₂ capture process applied in the cement industry.

References

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Figures

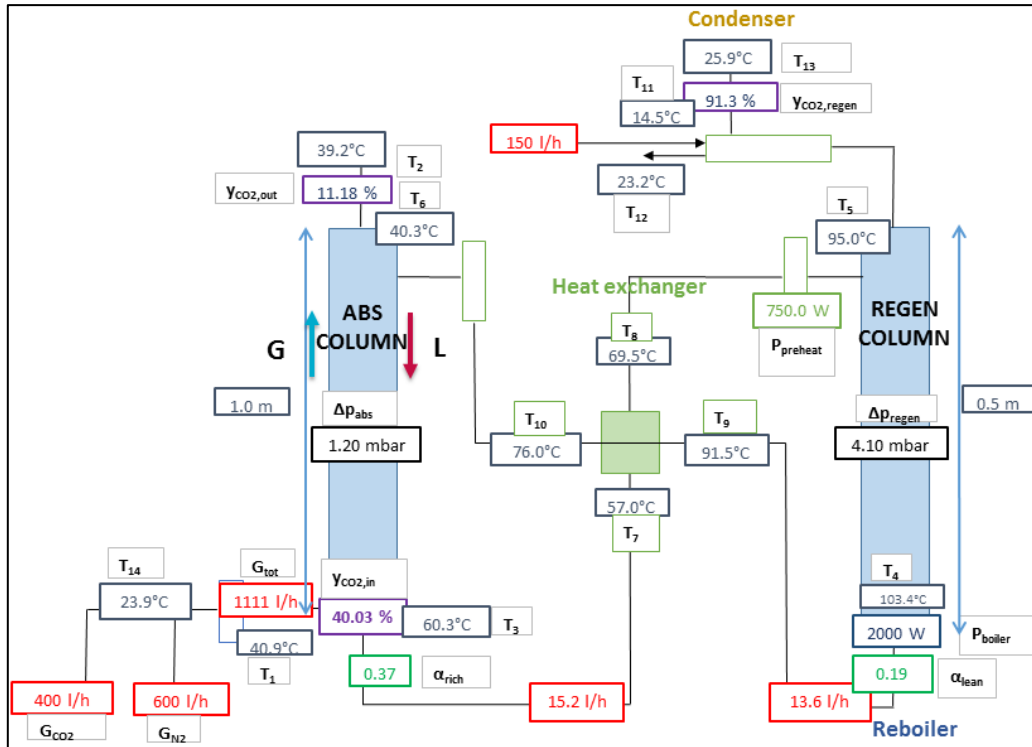


Figure 1: Scheme of the absorption-regeneration micro-pilot unit

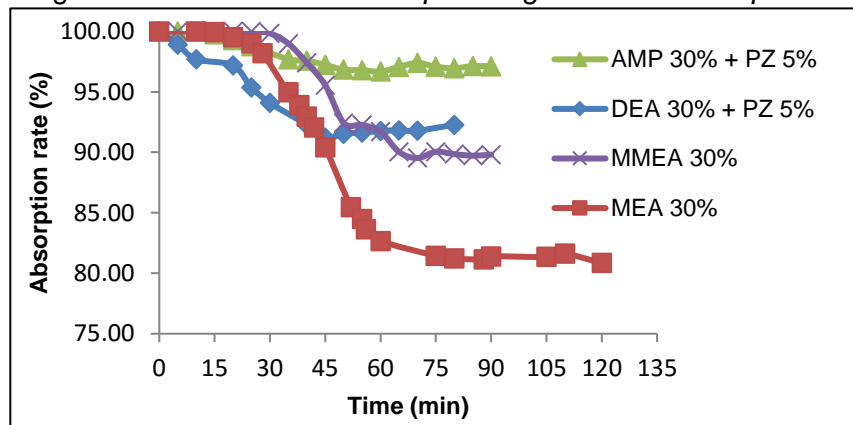


Figure 2: Best absorption performances at micro-pilot scale for $y_{CO_2, in}=40\%$ ($L= 14$ l/h; $G= 1111$ l/h)

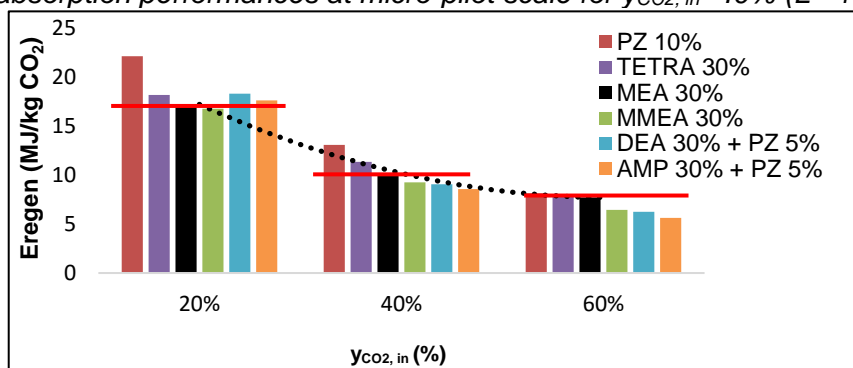


Figure 3: Comparison of the regeneration energies of the solvents for each $y_{CO_2, in}$