

# Study of two promising MOFs, MIL-91(Ti) and MIL-160(AI), for CO<sub>2</sub> capture from flue gas

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	Global overview	
General Context	Measurements and Methods	
For two decades, the reduction of anthropogenic CO <sub>2</sub> emissions from industries has become one of the most crucial issue to combat global warming. Shifting towards a low-carbon economy	<u>1) Pure CO<sub>2</sub> and N<sub>2</sub> adsorption isotherm measurements</u> performed with a homemade apparatus using a <u>Magnetic</u> <u>isotherm measurements after water pre-adsorption</u>	

needs cost-effective novel carbon capture utilization or sequestration (CCUS) solutions. Current benchmark technique, absorption-regeneration amine-based process, suffers from high energy penalties due to solvent regeneration and high environmental impacts. So, adsorption process is widely considered as a promising alternative. In this regard, MOFs as adsorbent offer tremendous potential, owing to their large CO<sub>2</sub> adsorption capacity and high CO<sub>2</sub> affinity. However, the performances of these materials have rarely been fully evaluated in real industrial conditions. In this context, this study focuses on the determination of performances on two promising MOFs, MIL-91(Ti)<sup>1</sup> and MIL-160 (AI)<sup>2,3</sup> in conditions close to real industrial conditions (presence of water, NOx, SOx...) for the purpose of being used in a **post-combustion capture** process based on a Vacuum Pressure Swing Adsorption (VPSA) process.

Suspension **Balance Rubotherm GmbH**<sup>4</sup> at several temperatures.

 $\rightarrow$  Working capacities, heat of adsorption (Clausius-Clapeyron), CO<sub>2</sub>/N<sub>2</sub> co-adsorption prediction (IAST<sup>5</sup>)

performed with DVS Vacuum provided by Surface Measurement Systems

 $\rightarrow$  Influence of water on CO<sub>2</sub> adsorption capacities

#### **Selected adsorbents** (p<sub>w</sub>=0.02 bar) conditions $\rightarrow$ Regenerability, CO<sub>2</sub> adsorbed amounts **MIL-91(Ti)** MIL-160(AI) Pressure 🖊 🔪 TiO(O<sub>3</sub>PCH<sub>2</sub>NHC<sub>4</sub>H<sub>8</sub>NHCH<sub>2</sub>PO<sub>3</sub>) $AI(OH)[C_4H_2O-(CO_2)_2]$ Column : h = 5 cm and d = 1 cm Oven $V = 3.9 \text{ cm}^{3}$ Chains of Ti octahedrons -Chains of Al octahedrons -Ligands phosponate Ligands 2,5-furan (PMDP) dicarboxylate (FDC) N<sub>2</sub> / He --- MFC $S_{BET} = 415 \text{ m}^{2}/\text{g}$ $S_{BFT} = 1220 \text{ m}^{2}/\text{g}$ Narrow pores (4.5 Å) N2 / CO2 - MFC Larger pores (6 Å) High degree of confinement **Rigid ligand** Flexible ligand Flowrate = 2 NL/h Highly hydrophilic Relatively less hydrophilic Mass spectrometer

#### 2) Breakthrough curves measurements

a) <u>CO<sub>2</sub>/N<sub>2</sub> (15/85)</u> breakthrough after He curves pressurization at 1 bar

### $\rightarrow$ CO<sub>2</sub>/N<sub>2</sub> selectivity and co-adsorption uptakes

b) <u>CO<sub>2</sub>/N<sub>2</sub> (15/85) adsorption/desorption breakthrough</u> curve cycles at 30°C and 1.1 bar under dry and humid 4) Operando analyses performed by coupling IR analysis of the gas phase in parallel with MS analysis under a flow containing contaminants (H<sub>2</sub>O, SO<sub>2</sub>, NOx, CO)

#### $\rightarrow$ Evaluation of the MOF stability and performance under real conditions

5) GCMC simulation performed to provide an *in-depth* microscopic understanding of CO<sub>2</sub> and N<sub>2</sub> co-adsorption behavior under dry and variable humidity conditions.

#### $\rightarrow$ Influence of water on CO<sub>2</sub> adsorption capacities $\rightarrow CO_2/N_2$ selectivity under dry and humid conditions

These 5 steps constitute the complete procedure set up within the framework of the MOF4AIR project for the selection of the best MOF candidates in powder form before the scaling and shaping steps for their use in VPSA process. The results section will focus on the results obtained during the first 3 steps.



	CO <sub>2</sub> adsorbed amount (mmol/g) at 0.15 bar and 303.15 K	CO <sub>2</sub> working capacity (mmol/g) at 303.15 K	∆h <sub>ads,</sub> CO <sub>2</sub> (kJ/mol)	∆h <sub>ads,</sub> N <sub>2</sub> (kJ/mol)
MIL-91(Ti)	1.25	1.10	36	20
MIL-160(Al)	0.97	0.85	33	20

#### **CO**<sub>2</sub> adsorption isotherms under dry and diverse humidity conditions







	CO <sub>2</sub> adsorbed amount (mmol/g)	N <sub>2</sub> adsorbed amount (mmol/g)	Exp CO <sub>2</sub> /N <sub>2</sub> selectivity range	IAST CO <sub>2</sub> /N <sub>2</sub> selectivity
MIL-91(Ti)	1.25 – 1.27	0.05 - 0.06	118 - 144	115
MIL-160(AI)	1.14 - 1.14	0.19 - 0.21	31 - 34	33

pressure

#### **Breakthrough curves: CO<sub>2</sub>/N<sub>2</sub> adsorption/desorption - Cyclability**





#### Observation of a 11% loss of adsorbed amounts for MIL-91(Ti) $\rightarrow$ Vacuum and/or heat required

0.15 bar and 298.15 K				
MIL-91(Ti)	1.64	0.72	-	-
MIL-160(AI)	1.24	1.09	1.08	0.97

## **Conclusions & Prospects**

These measurements highlight that MIL-91(Ti) has better performances than MIL-160(Al) in terms of working capacity and selectivity in dry conditions, however, MIL-160(Al) is less impacted by water and impurities maintaining these CO<sub>2</sub> adsorption properties under dynamic conditions. Moreover, MIL-160(Al) can be regenerated easily under humid conditions. These results highlight the need of measurements close to real conditions to properly select an adsorbent. MIL-160(AI) is therefore the first MOF selected in MOF4AIR project to be scaled-up and shaped for testing in VPSA process.

<u>References</u>		
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#### Complete regeneration for MIL-160(Al) without heat or vacuum



Observation of a 20% loss of adsorbed amounts for MIL-91(Ti)  $\rightarrow$  Vacuum and/or heat required Still complete regeneration for MIL-160(Al) without heat or vacuum

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