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1 Exhaust Gas Recirculation Cooler Fouling Morphology: 2 Characterisation, Spatiotemporal Nature, and System 3 Variable-Morphology-Property Correlation

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16 Abstract

17 Fouling is one of the primary causes of failure in exhaust gas recirculation (EGR)
18 coolers. Morphology may provide a powerful perspective for understanding the
19 mechanisms, behaviours, and properties of fouling. However, a systematic review of
20 fouling morphology is currently lacking. Considering the substantial progress made in
21 morphology-related studies within the industry in recent years, this work reviews the
22 findings on EGR cooler fouling morphology from four aspects: characterisation (scale,
23 object, category, and technique), spatiotemporal nature, variable-morphology
24 correlation, and morphology-property correlation. Furthermore, the current
25 challenges and opportunities in this field are discussed. Based on this, we propose a
26 framework for the morphological characterisation of EGR cooler fouling. It is
27 demonstrated that morphology plays a crucial role in revealing the spatiotemporal
28 characteristics of fouling, the formation and removal mechanisms, and the
29 correlations among system variables, morphology, and properties. Morphology still
30 holds significant potential in four areas: multi-scale and quantitative characterisation,
31 nomenclature and taxonomy, and full lifecycle evolution. The findings provide a
32 morphological perspective for fouling research within the industry and contribute to
33 advancing the science of fouling morphology.

34 **Keywords:** Morphology; Fouling; Characterisation; Spatiotemporal Nature; Exhaust
35 Gas Recirculation Cooler.

36 1. Introduction

37 Exhaust gas recirculation (EGR) cooling technology has become a key approach
38 for suppressing nitrogen oxide emissions from internal combustion engines due to its
39 dilution, thermal, and chemical effects [1, 2]. However, particulate deposition and
40 vapour condensation in exhaust gases form a complex mixture known as fouling [3, 4];
41 it is defined as the accumulation of unwanted deposits on surfaces [5]. Numerous
42 studies have reported that fouling leads to reduced heat transfer efficiency and
43 increased pressure drop [6, 7]; in severe cases, it may even result in complete blockage
44 [8, 9]. Therefore, the issue of fouling warrants significant attention.

45 Researchers in the industry have conducted extensive and in-depth reviews of
46 EGR cooler fouling. Hoard et al. [10] were the first to review the fundamental aspects
47 of this topic, including the concept, characteristics, deposition, stabilisation, and
48 recovery of fouling. Subsequently, Abd-Elhady et al. [11] expanded on this by
49 addressing additional critical topics, such as the functions of EGR coolers, descriptions
50 of fouling issues, their fundamental mechanisms, and the role of catalyst addition.
51 Abarham et al. [12] and Han et al. [13] not only focused on the deposition mechanisms
52 of fouling but also considered its removal mechanisms. Paz et al. [14] provided a
53 specialised report on the numerical modelling of fouling processes, while Yao et al. [4]
54 concentrated on reviewing the pathways of vapour condensation within coolers and
55 its consequences on fouling. These reviews collectively demonstrate that past studies
56 have systematically examined EGR cooler fouling from various perspectives, achieving
57 substantial progress.

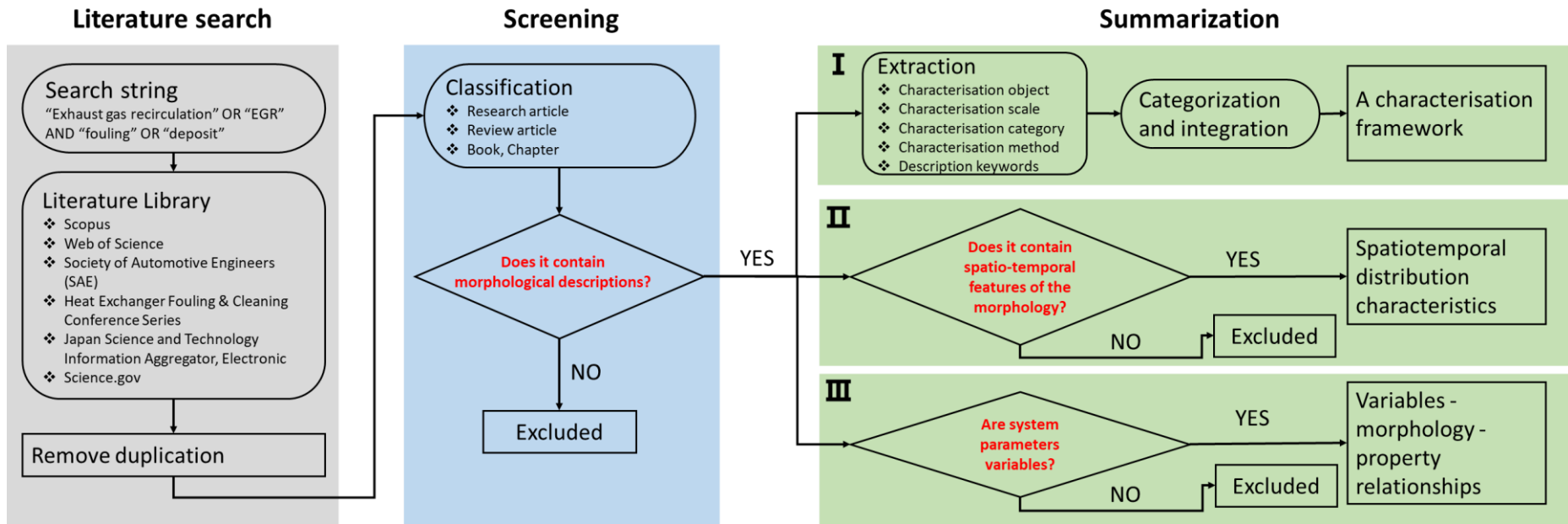
58 It has been observed that no retrospective studies on the morphology of EGR
59 cooler fouling currently exist. However, morphology plays a crucial role in analysing
60 fouling issues. At present, the industry commonly uses the thermal fouling resistance
61 curve to describe the three stages of fouling growth: the initiation phase, the
62 roughness-controlled phase, and the layer growth phase [15]. The advantage of this
63 method is that it allows for a rough understanding of fouling growth inside heat
64 exchangers through external monitoring of thermal resistance. However, this approach
65 is based on the correlation between fouling and thermal resistance, providing only
66 indirect evidence and failing to fully characterise the actual fouling growth process.
67 Morphology can address this limitation by directly observing and unbiasedly recording
68 the entire fouling growth process. For example, Løge et al. recently used high-
69 resolution X-ray micro-computed tomography to visualise the process of crystal
70 formation [16], revealing the complex process of multi-component mixed
71 crystallisation, which cannot be achieved by the thermal fouling resistance curve.
72 Beyond the growth process, morphology also provides valuable insights into other
73 fouling evolution processes. For instance, Paz et al. observed colour changes during
74 the ozone treatment of fouling to reflect the depth of the reaction between ozone and
75 fouling [3]. In summary, morphology offers a direct and clear perspective for
76 addressing fouling issues.

77 Given the importance of morphology and the current lack of systematic reviews

78 on EGR cooler fouling morphology, this study aims to comprehensively review the
79 progress in this field. The review covers four key aspects: morphological
80 characterisation (object, scale, category, and method, with a particular emphasis on
81 real-time in-situ characterisation), spatiotemporal distribution characteristics of
82 morphology, variable-morphology correlations, and morphology-property
83 correlations. Finally, the challenges and opportunities in this field are discussed. This
84 work not only systematically summarises the key findings in this area but, more
85 importantly, helps clarify the potential role of morphology in analysing fouling issues,
86 providing valuable references for future research.

87 **2. Methodology**

88 This work follows the process illustrated in [Figure 1](#), to discuss in detail four sub-
89 topics of fouling morphology. This process is also divided into literature search,
90 screening, and summarisation stages. The literature search section provides a detailed
91 account of the search strings and literature libraries used. The screening phase aims
92 to filter relevant publications. The summarisation phase synthesises key findings
93 related to the four sub-topics, namely: the characterisation framework,
94 spatiotemporal distribution characteristics, system variable-morphology correlations,
95 and morphology-property correlations.



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Figure 1. Flow of the overview for the EGR cooler fouling morphology

98 **3. Characterisation of fouling morphology**

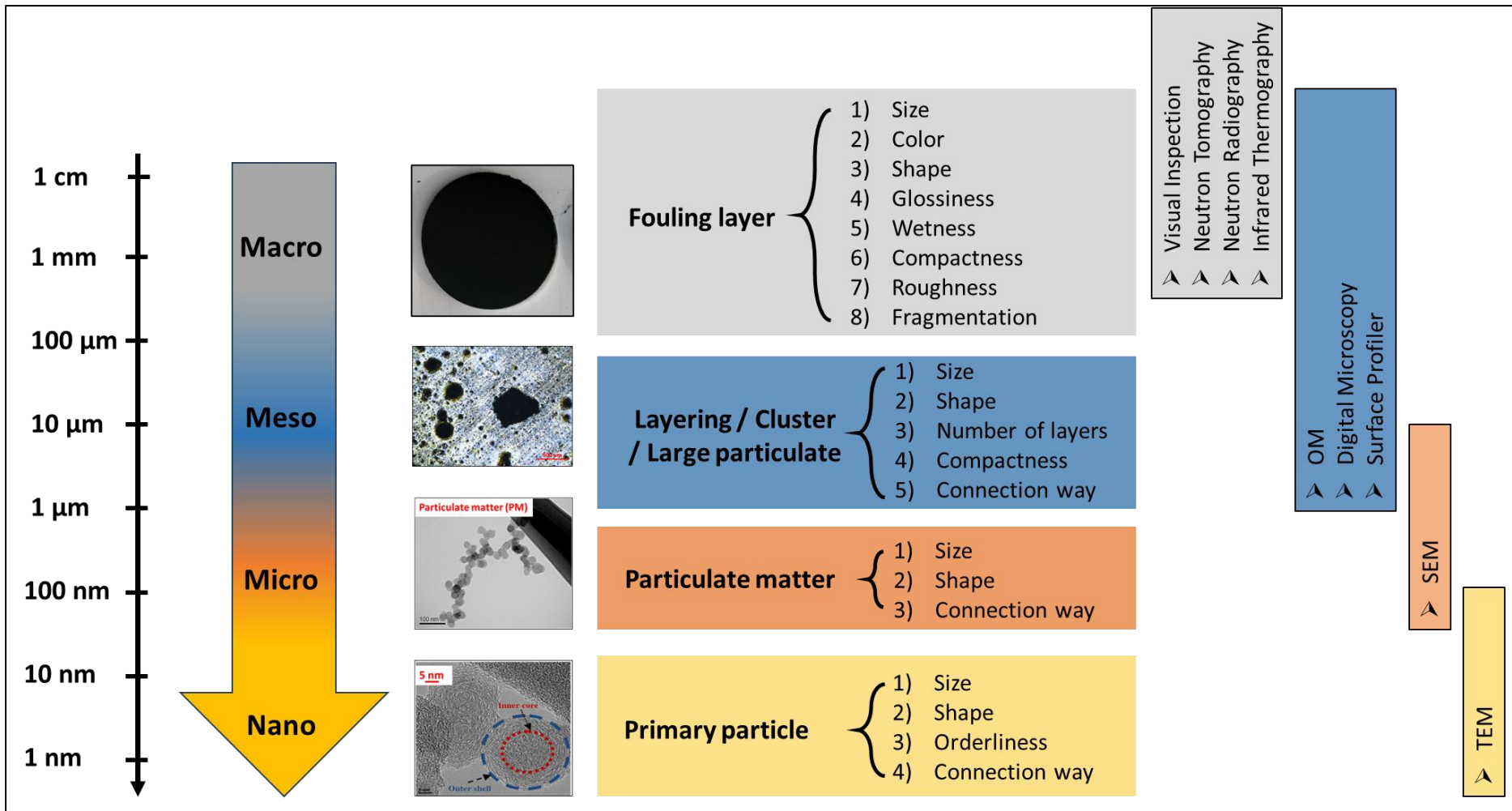
99 **3.1. A characterisation framework**

100 The meta-information extracted following the process outlined in [Figure 1](#) is
101 presented in [Table S1](#) of the supplementary document. Further refinement of this data
102 has yielded a characterisation framework for EGR cooler fouling morphology, as
103 illustrated in [Figure 2](#). This framework encompasses four key components:
104 characterisation scale, characterisation object, characterisation category, and
105 characterisation method.

106 Regarding the characterisation scale, spanning from centimetre to nanometre
107 levels, it can be further divided into four tiers: macroscopic, mesoscopic, microscopic,
108 and nanoscopic. Correspondingly, the four levels of characterisation objects are
109 distributed as follows: fouling layer, layering/cluster/large particulate, particulate
110 matter, and primary particle. For each characterisation object, this work has distilled
111 concise characterisation categories based on morphological descriptions from
112 previous publications. Taking the fouling layer as an example, comprehensive
113 characterisation can be conducted from eight categories: size, colour, shape, glossiness,
114 wetness, compactness, roughness, and fragmentation. More importantly, this
115 framework ultimately provides characterisation methods applicable to different scale
116 levels and objects.

117 It is important to note that there is no strict correspondence between the four
118 levels of characterisation objects and methods. This is because more advanced
119 characterisation techniques often have downward compatibility. For instance,
120 Scanning Electron Microscopy (SEM) can cover part of the working range of Optical
121 Microscopy (OM), while Transmission Electron Microscopy (TEM) can, under certain
122 conditions, partially replace SEM. Consequently, for the same characterisation
123 category of a given object, multiple characterisation techniques may be available. For
124 example, when the fouling volume is sufficient, qualitative observation of the fouling
125 layer's roughness can be achieved through visual inspection or OM-based observation.
126 This principle applies to other characterisation categories as well.

127 In summary, the proposed characterisation framework comprehensively
128 addresses the aspects involved in EGR cooler fouling morphology characterisation,
129 whilst, clearly delineating typical hierarchical levels. This framework serves as a
130 valuable reference for future practitioners, reducing their exploratory time and
131 enabling them to more effectively achieve their morphological characterisation
132 objectives. Additionally, it facilitates more efficient intra-industry communication
133 among practitioners, enhancing the accuracy of dialogue. Most crucially, this shared
134 characterisation framework provides a solid foundation for further understanding the
135 temporal evolution and spatial distribution patterns of fouling, as well as the
136 correlations between variables, morphology, and properties.



137

138

139

Figure 2. A characterisation framework (including characterisation scale, object, category, and technology) for the EGR cooler fouling morphology

140 **3.2. In situ and real-time characterisation**

141 Morphological characterisation is typically conducted by mechanically dissecting
142 fouled coolers to expose the fouling, thereby facilitating the observation of its
143 morphology, such as described in [17-19]. However, considering that environmental
144 changes during the spatial relocation involved in sampling and preparing fouling
145 specimens may damage their morphology and result in the loss of original features, in-
146 situ characterisation has become a key topic of interest in the field. Similarly, fouling
147 samples may undergo morphological evolution due to time-sequential events such as
148 preparation, storage, and transportation following the fouling incident. As a result,
149 real-time characterisation has also emerged as a prominent subtopic. Although in-situ
150 and real-time characterisation focuses on spatial and temporal dimensions,
151 respectively, real-time characterisation generally satisfies the requirements of in-situ
152 characterisation as well.

153 The implementation of in-situ and real-time characterisation can be broadly
154 divided into two strategies. The first involves using traditional experimental platforms
155 combined with advanced optical techniques for characterisation. The second strategy
156 upgrades experimental platforms to enhance accessibility while integrating
157 characterisation technologies. For the first approach, Ismail et al. pioneered the
158 development of the neutron radiography technique to perform in-situ, non-
159 destructive measurements of fouling morphology, providing an accurate
160 representation of fouling thickness and contours [20]. Similarly, Lance et al. employed
161 neutron tomography to conduct in-situ tests of fouling morphology, achieving three-
162 dimensional reconstructions of its structure [21]. For the second approach, Abarham
163 et al. developed a visualised experimental platform combined with a digital
164 microscope to record, in situ and in real-time, the morphological evolution of fouling
165 during its formation or removal [22, 23]. Likewise, Salvi et al. utilised a visualised
166 experimental platform along with optical and infrared testing techniques to achieve
167 in-situ and real-time characterisation of the three-dimensional morphology of fouling
168 [24].

169 **4. The spatiotemporal distribution characteristics**

170 **4.1. Evolution of the fouling morphology**

171 This section provides a comprehensive review of previous studies that have
172 elucidated the generation, growth, and evolution processes of fouling in EGR coolers
173 from a morphological perspective. It also examines how these studies contribute to
174 our understanding of fouling mechanisms.

175 Firstly, morphological characterisation techniques effectively reveal the initial
176 formation of fouling. Tanaka et al. observed protrusions on a stainless steel surface
177 after 1 minute and 10 seconds, indicating the onset of fouling. The original images
178 vividly illustrate the initial morphology of fouling formation. Furthermore, they
179 monitored morphological changes over 16 minutes. Following the formation of hard

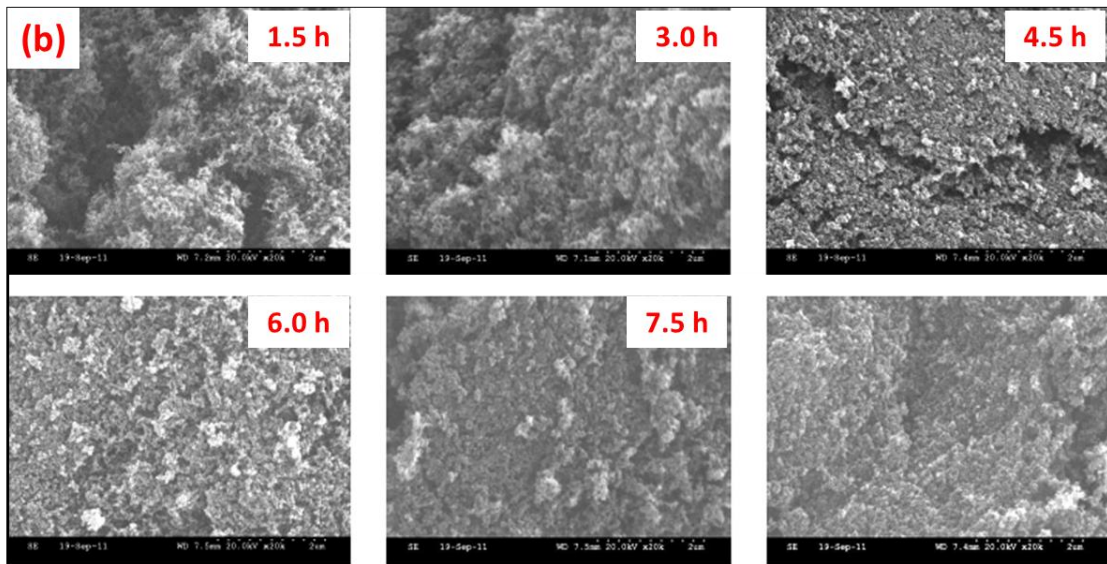
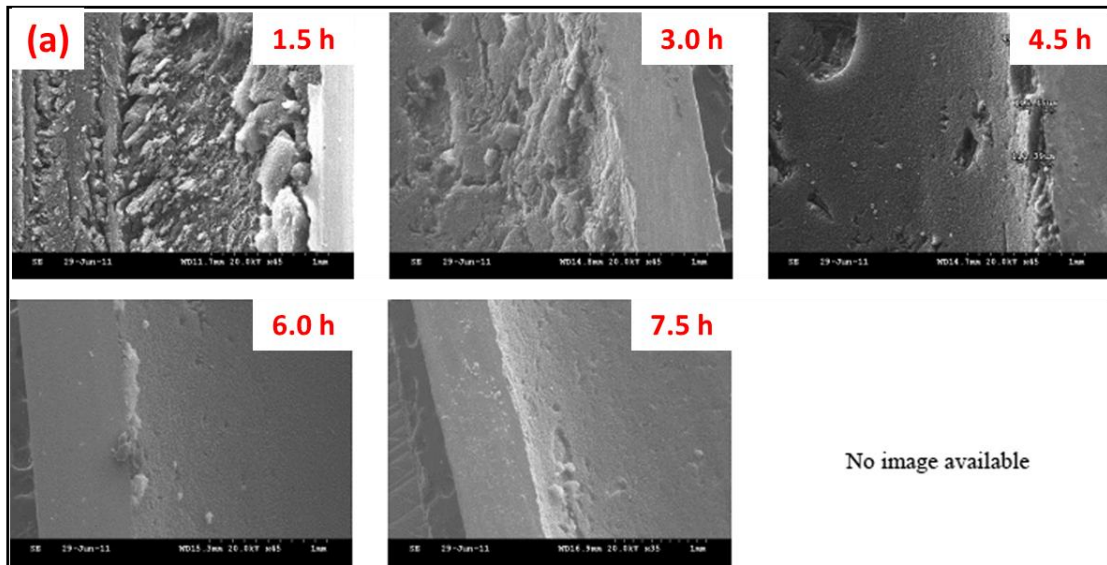
180 fouling at 1 minute 10 seconds, particles continuously deposited and covered the hard
181 fouling surface, creating a porous, powder-like deposit that continued to grow,
182 eventually enveloping the underlying hard fouling completely [25]. This study
183 meticulously documents the gradual growth process of fouling.

184 Li et al. provided detailed observations on how fouling growth progresses "from
185 points to surfaces". Initially, particles with diameters of about tens of micrometres
186 were scattered across the wall surface. As more particles are deposited, the size of
187 these wall particles gradually increases. Individual particles began to be enveloped and
188 started connecting with nearby particles. Eventually, after 1.5 hours, larger "dune-like"
189 structures (approximately 50 μm or larger in length) were formed [26].

190 In addition to early-stage fouling observations, researchers have also investigated
191 fouling morphology over longer time scales. Tanaka et al. used scanning electron
192 microscopy to observe changes in fouling thickness over 24 hours period. They found
193 that the thickness of both types of fouling increased linearly with time [25]. Li et al.
194 compared fouling morphology at 22.5 hours and 31.5 hours. The authors noted that
195 from around 22 hours into the experiment, the dune-like structures on the fouling
196 surface began to disappear, and the surface morphology became smoother [26].

197 To quantify the degree of surface roughness in fouling, Li et al. introduced a
198 parameter called the area ratio, defined as the ratio of the actual surface area to the
199 corresponding projected area. They observed a decrease in the area ratio from 115%
200 to 100% at 6.5 h, and 37 h, respectively, further corroborating the gradual smoothing
201 of the surface morphology [26]. In a subsequent study by the same team, they
202 employed a similar parameter, the SA ratio, defined as the ratio of the surface area of
203 the deposit to the surface area of a comparable flat plate. Contrary to their earlier
204 findings, they discovered that the SA ratio increased over time, possibly due to partial
205 fouling agglomeration or the presence of large particles [27]. The introduction of these
206 quantifiable parameters has undoubtedly enhanced the characterisation of fouling
207 morphology, moving beyond mere qualitative descriptions.

208 Contradictory results regarding the temporal evolution of fouling morphology
209 have also emerged in two other studies. Prabhakar and Boehman examined fouling
210 morphology at different time intervals using low and high magnification, as shown in
211 **Figure 3**. They observed that at 1.5 h, particles were randomly deposited on the tube
212 surface. As time progressed, more particles accumulated on the existing layer,
213 resulting in a completely covered and smooth, dense surface at 7.5 h [28]. In contrast,
214 a recent quantitative study by Paz et al. measured surface roughness in three cases at
215 1.5 h, 3 h, 6 h, and 9 h. They found that roughness increased over time in all areas,
216 particularly near the exhaust outlet, where roughness at 9 h was 2-3 times higher than
217 at 6 h [29]. Broadly speaking, these findings suggest that fouling roughness can either
218 decrease or increase over time, highlighting the complexity of this phenomenon.



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Figure 3. Variation of fouling microstructure as a function of time. (a) low magnification, (b) high magnification [28]

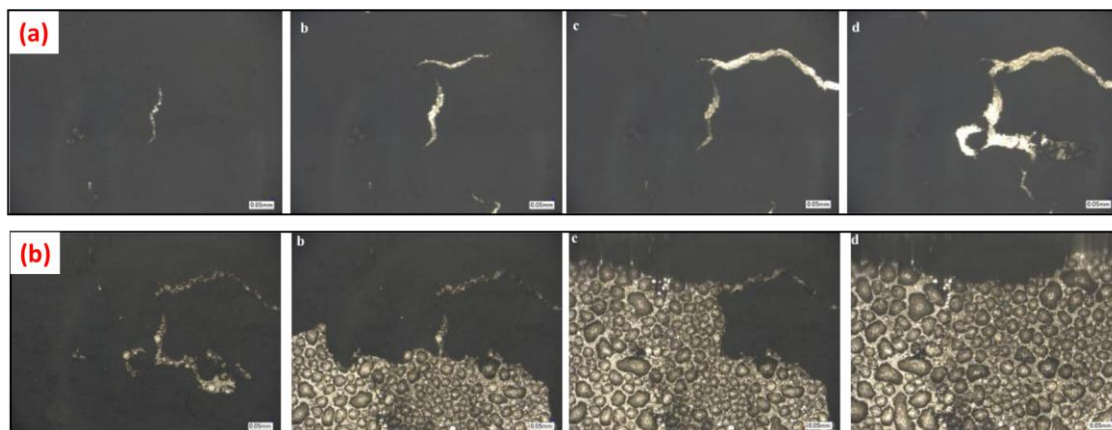
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It is noteworthy that in the study by Prabhakar and Boehman, they established a correlation between morphological visual evidence and the heat exchange efficiency of coolers. They posited that once fouling completely covers the tube walls, the cooler's heat exchange efficiency begins to approach a certain value and remains stable [28]. This method of establishing connections further corroborates that, compared to indirectly reflecting fouling growth through parameters such as total thermal resistance or thermal efficiency, the morphological perspective not only provides a more intuitive approach but also offers a more fundamental interpretation for indirect methods.

231
232
233

In addition to the aforementioned morphological studies focusing on fouling formation and growth processes, several investigations have specifically examined the morphological changes during fouling removal [22, 23, 30]. For instance, in Furuhata

234 et al.'s study, at 5 h, water vapour penetrated through the loose surface layer of fouling,
235 condensing within the fouling layer. This caused the fouling to expand, elevating the
236 surface layer, which subsequently detached under the influence of airflow. By 6 h, the
237 expanded fouling had disappeared [30]. Similarly, Abarham et al. provided a more
238 detailed account of the morphological changes during the formation of cracks before
239 fouling removal and during the detachment process itself. As illustrated in **Figure 4**,
240 these processes occur rapidly, typically completing crack growth and partial fouling
241 detachment within 5 minutes. During this period, the morphology of the fouling is
242 almost entirely transformed [22, 23].



243

244 **Figure 4.** Cracks in fouling. Flow direction from left to right. (a) five-minute interval
245 between successive images at 42°C, (b) one-minute interval between successive
246 images at 20°C [23]

247 In conclusion, the morphology of fouling evolves over time, potentially becoming
248 smoother or rougher, with surface undulations that may increase or decrease.
249 Currently, there is no definitive consensus on these changes, necessitating further
250 research to elucidate these controversies. However, there is agreement that when
251 fouling is stripped away, the fragmentation of fouling rapidly increases. More
252 significantly, the analysis of these results demonstrates that the characterisation of
253 fouling morphology provides direct and compelling evidence for interpreting the
254 processes of fouling generation, growth, removal, and stabilisation. This approach
255 offers valuable insights into the complex dynamics of fouling phenomena.

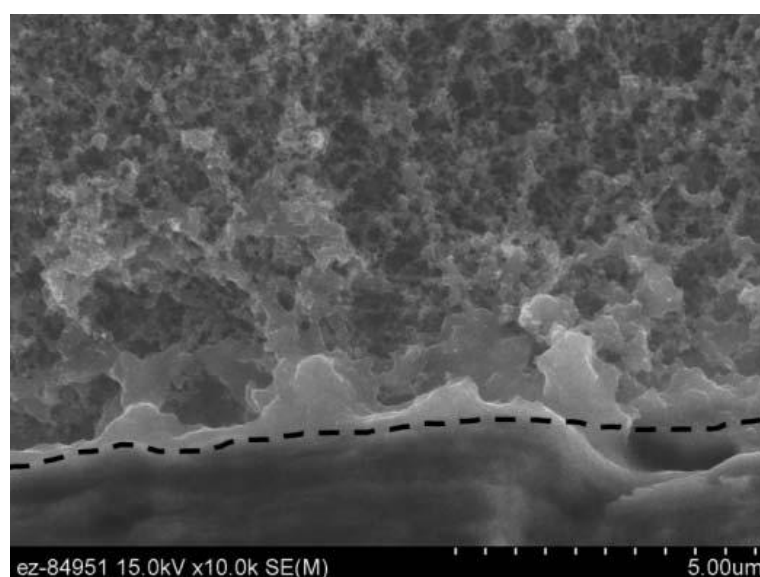
256 **4.2. Spatial distribution of fouling morphology**

257 Spatial variations in fouling morphology manifest primarily in two aspects:
258 microscopic differences across different layers in the cross-section and macroscopic
259 differences along the direction of gas flow. The following sections provide a
260 comprehensive summary of these morphological distribution characteristics in both
261 dimensions.

262 The fouling cross-section consists of material between two characteristic
263 interfaces: the gas-fouling interface and the fouling-tube interface. Styles et al.
264 discovered that fouling can be divided into two layers: a highly dense hydrocarbon

265 layer near the fouling-tube interface, and a particulate layer with a hydrocarbon
266 distribution gradient further from this interface. This gradient is visually evident as a
267 transition from dark near the gas-fouling interface to lighter near the fouling-tube
268 interface [31]. Lance et al.'s research provided more intuitive evidence, revealing that
269 the reflectivity of fouling is highest near the fouling-tube interface and gradually
270 decreases towards the gas-fouling interface. This is due to variations in hydrocarbon
271 condensation caused by thermal gradients within the fouling layer, with lower
272 temperatures at the fouling-tube interface resulting in higher concentrations of
273 condensed hydrocarbons. Consequently, fouling near the fouling-tube interface is
274 more moist and dense, while fouling near the gas-fouling interface is drier and more
275 porous [32]. Another study by Lance et al. found that fouling near the gas-fouling
276 interface is significantly finer and less dense [17]. Tanaka et al.'s experimental results
277 also confirmed this morphological difference, terming the fouling near the gas-fouling
278 interface as a "powdery deposit" and that near the fouling-tube interface as a "lacquer
279 deposit" or "hard deposit". Despite the nearly identical original composition of both
280 layers, the former exhibits a highly porous structure, while the latter presents a dense
281 structure [18].

282 The layered phenomenon of fouling has prompted researchers to observe its
283 internal connecting structure through morphological methods. As shown in **Figure 5**,
284 in addition to the significant density differences observed in the cross-section of
285 fouling, it is evident that the dense and loose layers of fouling are typically connected
286 by columnar structures [33]. Although different studies have varying nomenclature for
287 the fouling layers, the findings consistently show that the top layer of fouling is
288 supported on the bottom layer by multiple columnar structures [25, 32].



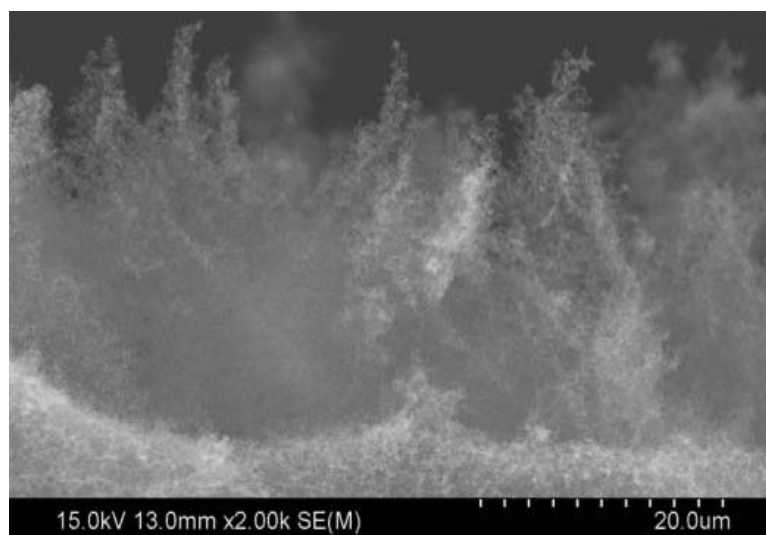
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Figure 5. Fouling interlayer columnar connections [33].

290

291 It is worth noting that, unlike other areas, the morphology of fouling at the gas-

292 fouling interface is particularly distinctive. **Figure 6** illustrates the fouling morphology
293 at the gas side at 2,000x magnification, presenting a dendritic structure referred to as
294 dendrites. These dendrites, approximately several tens of micrometres in height, are
295 formed by the aggregation of particles and incline in the direction of waste gas flow
296 [33]. These dendrites are highly porous internally, resembling fluffy cotton, and are
297 dispersed at the gas-fouling interface [25, 34]. However, Storey et al. suggest that such
298 morphologies are not observed on fouling layers with high hydrocarbon content [33].



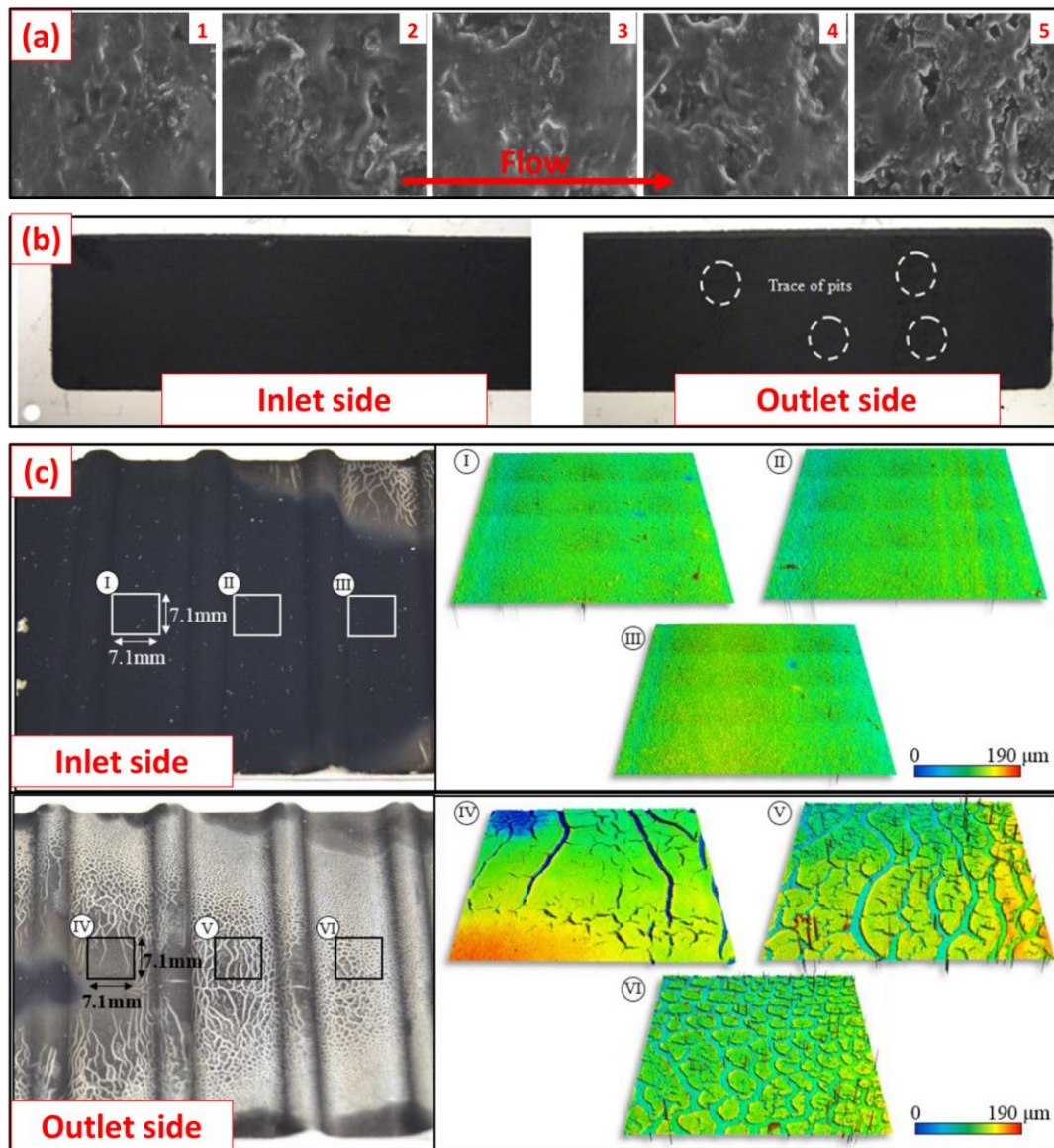
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300 **Figure 6.** Dendritic form of fouling in the gas-fouling interface (2 KX) [33].

301 Based on the comparison of fouling cross-sectional morphologies, significant
302 differences in glossiness, wetness, and compactness exist among different layers. This
303 is because the temperature at the fouling-tube interface is lower than that at the gas-
304 fouling interface, which is more conducive to hydrocarbon condensation. The
305 condensed hydrocarbons, in turn, alter the morphology of the fouling. Interestingly,
306 this research demonstrates how the differences in fouling morphology can be used to
307 inversely deduce the degree of involvement of various fouling mechanisms,
308 particularly reflecting the extent of hydrocarbon condensation within the fouling.

309 Along the gas flow direction, the overall morphology of fouling exhibits an
310 increasing trend in roughness. As shown in **Figure 7 (a)**, Tian et al.'s experimental
311 results demonstrate that from upstream to downstream of the cooler, the fouling
312 morphology continuously changes, with downstream locations showing rougher
313 fouling and more pronounced grooves [35]. In the same year, Al-Janabi and Malayeri
314 observed that fouling at the inlet of a smooth plate was more uniform, while fouling
315 in the middle and outlet areas was more uneven, with scratches and grooves
316 appearing [36], as illustrated in **Figure 7 (b)**. Paz et al. employed more advanced testing
317 methods to showcase three-dimensional surfaces of fouling at different cooler
318 locations, as depicted in **Figure 7 (c)**. The results indicate that fouling at the inlet is very
319 smooth, while the fouling surface at the outlet exhibits mud cracks. They attributed
320 this morphological difference to structural changes in fouling caused by the

321 condensation and evaporation of hydrocarbons [37]. In another study, they
 322 quantitatively compared the roughness of the same parts of the fins (the windward
 323 side of the fin foot) at the cooler inlet and outlet, finding that the roughness at the
 324 outlet was greater compared to the inlet [29].

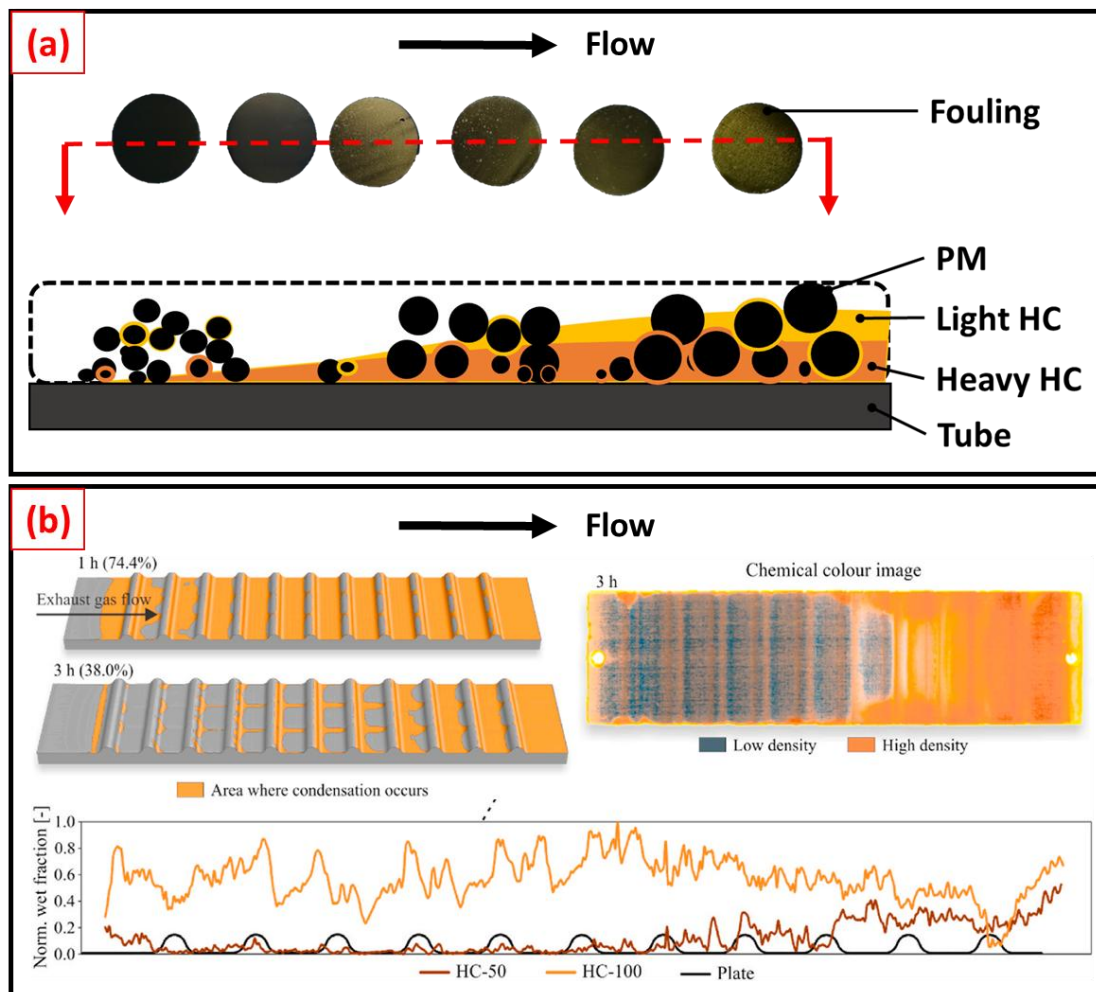


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326 **Figure 7.** Fouling roughness distribution along the airflow direction. (a) Tian et al.
 327 [38], (b) Al-Janabi and Malayeri [36], (c) Paz et al. [37].

328 Fouling colour also changes along the gas flow direction. Han et al. observed that
 329 due to the continuous temperature decrease along the gas flow direction, the colour
 330 of the fouling gradually deviates from black at the outlet compared to the black fouling
 331 composed of dry carbon soot at the inlet. This is attributed to the intensified
 332 condensation of heavy hydrocarbons [39], as shown in **Figure 8 (a)**. Vence et al.'s
 333 experimental results corroborated this observation, as illustrated in **Figure 8 (b)**, where

334 the chemical colouration and wet fraction of fouling increase along the gas flow
 335 direction. This phenomenon stems from the lower downstream temperatures, leading
 336 to increased hydrocarbon condensation and, consequently, colour variations [40].



337
 338 **Figure 8.** Fouling chemical colour distribution along the airflow direction. (a) Han et
 339 al. [39], (b) Vence et al. [40].

340 Beyond surface morphology differences along the gas flow direction, variations
 341 in cross-sectional morphological details have also been identified. Lance et al.
 342 confirmed that compared to the inlet, the middle section of fouling exhibits an
 343 increase in shiny layers, indicating more hydrocarbon condensation [17]. Paz et al.'s
 344 findings align with this, revealing that fouling at the outlet contains more oily
 345 substances compared to dry fouling at the inlet [37]. Yoo et al. compared the top layer
 346 morphology of fouling at the front, middle, and rear of the cooler. They discovered
 347 that dendrites grow larger and taller along the gas flow direction. This was attributed
 348 to the reduction in effective exhaust gas flow area as fouling accumulates, resulting in
 349 increased gas velocity and shear force at the gas-fouling interface. Consequently,
 350 dendrites at the interface tilt and break, developing into larger and taller structures
 351 [34]

352 Fouling morphology exhibits significant variations along the gas flow direction,
 353 specifically in terms of roughness, colour, glossiness, and dendrite size. These
 354 differences provide crucial evidence for interpreting fouling mechanisms: roughness
 355 changes may reflect the impact of large particle impingement and hydrocarbon
 356 condensation; colour and glossiness variations may indicate changes in hydrocarbon
 357 condensation intensity; dendrite size differences may reflect the interplay between
 358 removal and deposition mechanisms at the interface.

359 This section comprehensively reviews the temporal and spatial distribution
 360 characteristics of fouling morphology. From a temporal perspective, morphological
 361 changes effectively reflect the generation, growth, removal, and stabilisation
 362 behaviours of fouling. From a spatial perspective, morphology provides important
 363 evidence for decoding fouling deposition and removal mechanisms.

364 5. The system variable – morphology correlation

365 **Table 1** provides a concise summary, in chronological order, of the 22 past studies
 366 identified in this work that investigated the correlation between system variables and
 367 fouling morphology. It can be observed that the system variables involved are quite
 368 extensive, including cooler structure, flow rate, engine operating conditions, coolant
 369 temperature, engine start-up mode, mass flow rate, baking temperature, fuel type,
 370 wall temperature, soot concentration, hydrocarbon concentration, inlet gas
 371 temperature, and O₃ concentration. Based on the physical nature of these variables
 372 and the frequency of their investigation, flow rate, temperature, and exhaust gas
 373 components are identified as the three main influencing variables. These variables are
 374 reviewed in detail below.

375 **Table 1**

376 Summary of the investigation on the correlation between system variables and
 377 morphology categories for exhaust gas recirculation coolers fouling

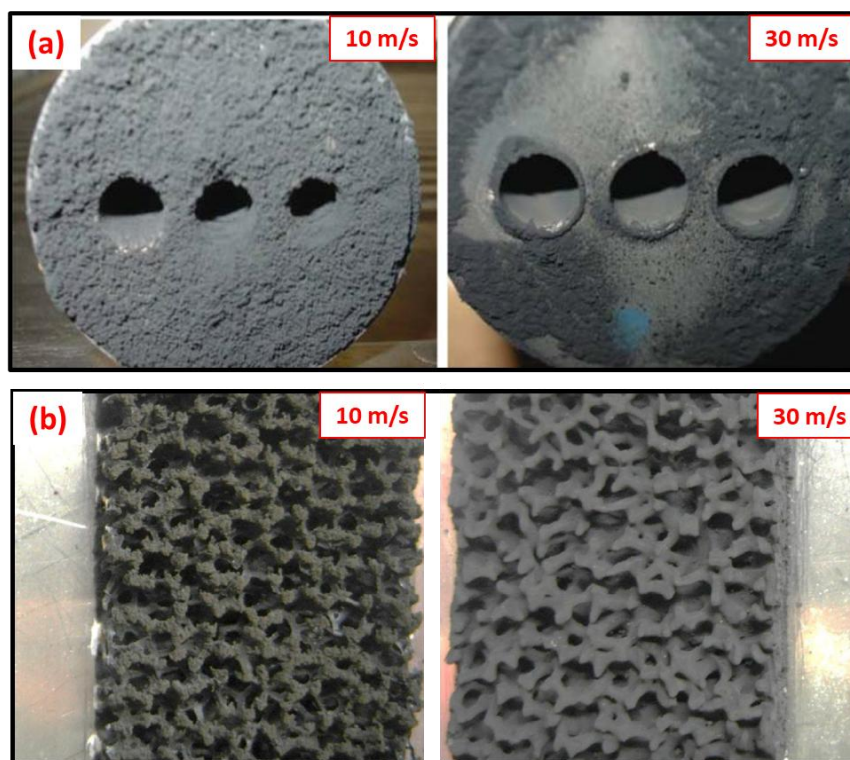
Reference	Year	System variable	Fouling morphology category
Ismail et al. [41]	2004	Cooler inlet header structure	Roughness
Abd-Elhady et al. [42]	2011	Flow rate	Thickness of fouling
Jang et al. [43]	2011	Cooler structures	Wetness
Malayeri et al. [44]	2013	Flow rate	Compactness; Size of particulate matter
Bravo et al. [45]	2013	Cooler structures	Wetness
Bravo et al. [46]	2013	Engine operation points	Compactness
Prabhakar and Boehman [28]	2013	Coolant temperature	Roughness
		Engine operation	Size and number of void

		condition	
Sluder et al. [47]	2014	Mass flow	Roughness
Kuhara et al. [48]	2014	Engine start mode	Roughness; Number of voids
Salvi et al. [49]	2014	Baking temperature	Roughness (Area ratio); Thickness of fouling
Arnal et al. [50]	2015	Fuel type	Orderliness of primary particle
Tanaka et al. [18]	2016	Wall temperature	Shape; Glossiness; Compactness
Hooman and Malayeri [51]	2016	Flow rate	Roughness
Matsudaira et al. [52]	2017	Cooler structures	Distribution state
Arnal et al. [53]	2018	Not reported	Orderliness of primary particle
Lance et al. [54]	2018	Soot concentration	Size of the primary particle; Porosity of primary particle
Paz et al. [37]	2019	Hydrocarbon concentration	Wetness; Glossiness
Paz et al. [29]	2021	Hydrocarbon concentration	Shape of primary particles; Roughness
Bera et al. [55]	2022	Heat temperature	Shape; Glossiness; Compactness
Li et al. [56]	2022	Hydrocarbon concentration	Size of dendritic structures; Thickness of fouling
Tomuro et al. [57]	2023	Coolant Temperature; Inlet gas Temperature	Compactness; Fragmentation
Vence et al. [40]	2023	Hydrocarbon concentration	Color; Wetness
Vence et al. [58]	2023	O ₃ concentration	Color; Wetness

378 **5.1. Effect of flow rate**

379 The consequence of exhaust gas velocity or mass flow rate on fouling morphology
380 is illustrated in **Figure 9**. Malayeri et al. compared fouling characteristics at two flow
381 velocities, 10 m/s and 30 m/s, as shown in **Figure 9 (a)**. They observed that fouling

382 formed at 10 m/s was more porous and had coarser particles [44]. Beyond
383 conventional EGR coolers, Hooman and Malayeri examined the differences in fouling
384 morphology for metal foam EGR coolers at 10 m/s and 30 m/s, as depicted in **Figure 9**
385 **(b)**. Their findings revealed that fouling at lower flow velocities was discontinuous and
386 rough, whilst, at higher velocities, it was continuous and smooth [51]. Sluder et al.'s
387 experimental results also confirmed that higher mass flow rates produce more uniform
388 fouling [47]. Generally, higher gas velocities result in greater shear forces at the gas-
389 fouling interface, leading to stronger fouling removal effects [12, 13, 19, 59].
390 Consequently, the morphological differences caused by flow velocity provide crucial
391 evidence for understanding fouling removal mechanisms.



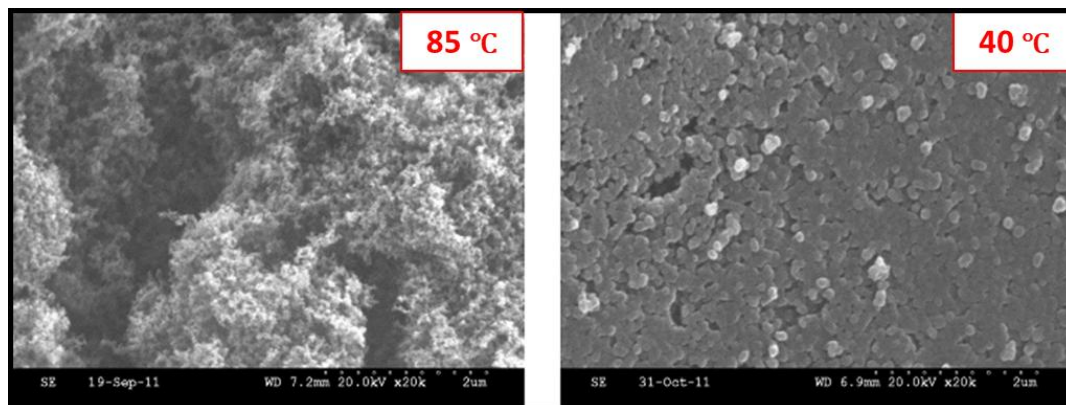
392

393 **Figure 9.** Effect of gas flow rate on fouling morphology. (a) Malayeri et al. [44], (b)
394 Hooman and Malayeri [51].

395 5.2. Effect of temperature

396 Multiple studies have demonstrated that the cooler wall temperature
397 significantly influences fouling morphology. As illustrated in **Figure 10**, Prabhakar and
398 Boehman observed that fouling generated at 85 °C was rougher than that formed at
399 40 °C [28]. Tanaka et al. categorised fouling into distinct types based on formation
400 temperature: 'soft deposit' at room temperature, 'low-temperature lacquer' at 80 °C,
401 and 'high-temperature lacquer' at 100 °C, whilst no fouling occurred at 120 °C [18].
402 Although these two studies employed different morphological characterisation
403 classifications, both indicated that variations in formation temperature affect fouling
404 morphology. This consequence likely stems from temperature's strong influence on

405 thermophoretic deposition and hydrocarbon condensation processes [12, 60, 61].
406 Therefore, the morphological differences caused by formation temperature provide
407 valuable insights into understanding particulate matter deposition and condensation
408 mechanisms.

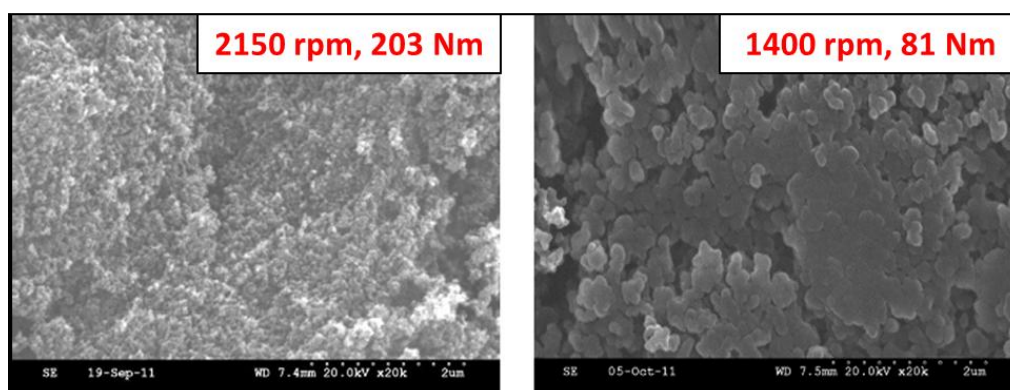


409

410 **Figure 10.** Effect of wall temperature on fouling morphology. From Prabhakar and
411 Boehman [28]

412 5.3. Effect of exhaust gas components

413 Fouling consists of particulate matter deposition and vapour condensation from
414 exhaust gases. Consequently, fouling morphology is significantly influenced by exhaust
415 composition, which is directly governed by engine operating conditions. Based on this,
416 researchers have compared the effect of engine load on fouling morphology.
417 Prabhakar and Boehman compared fouling morphologies under two engine operating
418 conditions (2150 rpm, 203 Nm and 1400 rpm, 81 Nm), as shown in **Figure 11**. They
419 found that fouling under 203 Nm conditions had more numerous and finer pores,
420 while fouling under 81 Nm conditions had larger but fewer pores [28]. Kuhara et al.
421 compared fouling morphologies under cold start and hot start conditions. Results
422 showed that fouling surfaces were smoother under cold start conditions, while hot
423 start conditions produced fouling surfaces with more irregularities and pores [48].

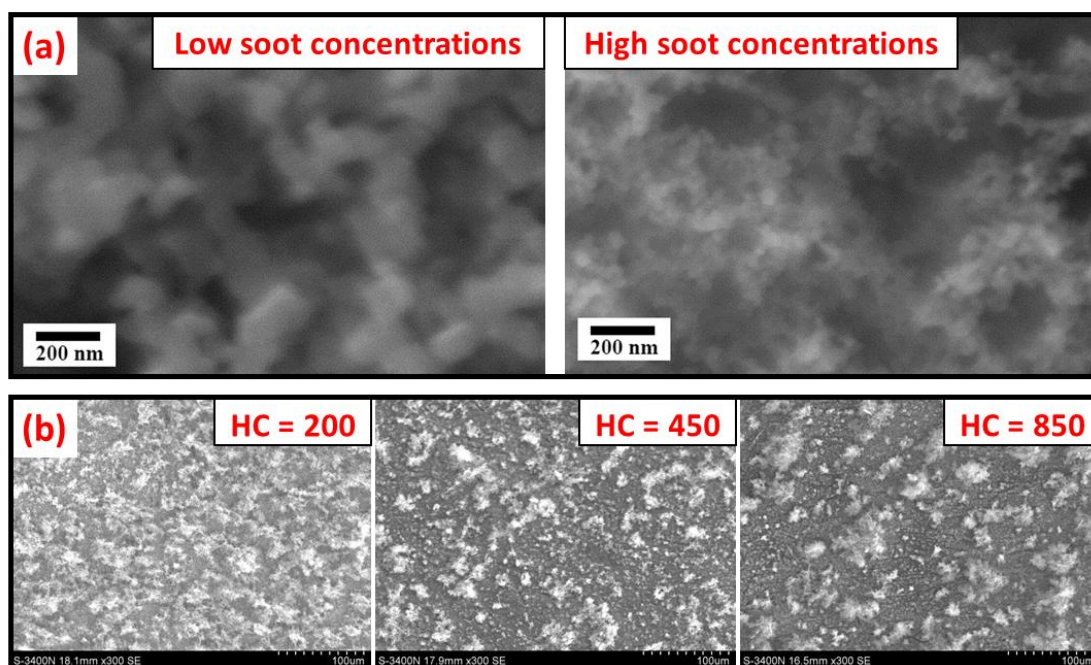


424

425

Figure 11. Effect of engine load on the fouling morphology [28]

426 Since changes in engine operating conditions involve simultaneous alterations of
427 multiple key parameters (HC composition and concentration, soot concentration and
428 size distribution, temperature, flow rate, etc.), it represents a composite external
429 control variable. This approach makes it challenging to identify the influence of
430 individual parameters on fouling morphology. Therefore, some researchers have
431 adopted a single-variable approach to further investigate these issues. Lance et al.
432 compared fouling morphologies under low and high soot concentration conditions, as
433 shown in **Figure 12 (a)**. Results indicated that compared to low soot concentrations,
434 high soot concentrations produced fouling with smaller primary particles and higher
435 porosity [54]. Li et al. compared the influence of another key parameter - HC
436 concentration on fouling morphology, as shown in **Figure 12 (b)**. They found that
437 higher HC concentrations resulted in fewer but larger dendritic structures on the
438 fouling surface due to enhanced particle agglomeration by the high concentrations of
439 condensed hydrocarbons [56].



440

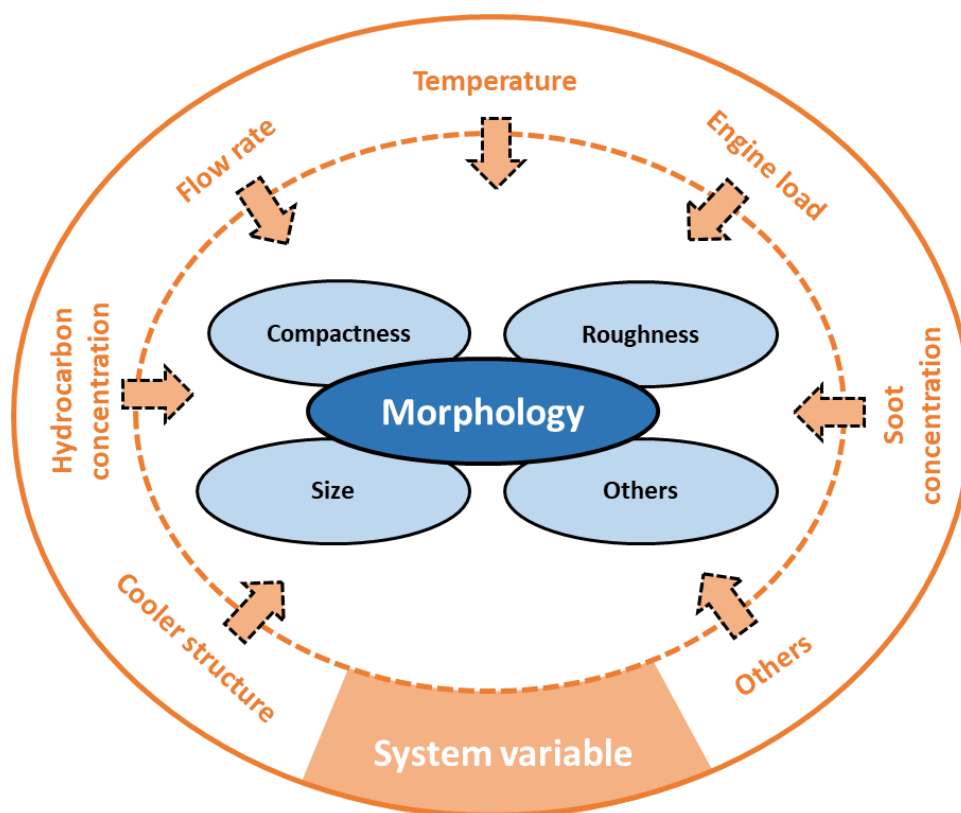
441 **Figure 12.** Effect of components of exhaust gas on the fouling morphology. (a) soot
442 concentration [54], and (b) Hydrocarbon concentration [56]

443 This series of experiments exploring the correlation between exhaust
444 composition and fouling morphology reveals the close relationship between fouling
445 morphology and its constituent components. The results demonstrate that fouling
446 morphology is highly correlated with the composition and proportion of particulate
447 matter and hydrocarbons that constitute the fouling. Specifically, different
448 compositions and proportions lead to different fouling morphologies. Furthermore,
449 the introduction of condensed hydrocarbons further complicates this process,
450 triggering more complex coupling effects. For instance, agglomeration effects caused
451 by liquid-phase forces can make fouling structures more compact and smoother.

452 Therefore, studying the relationship between exhaust composition and fouling
453 morphology not only helps understand fouling formation mechanisms but also
454 provides new avenues for quantifying the contribution of each sub-component to
455 fouling morphology.

456 In addition to the aforementioned system variables affecting fouling morphology,
457 differences in cooler structures can also lead to the formation of different fouling
458 morphologies [43, 52]. This is primarily due to changes in exhaust gas flow patterns
459 caused by different structures, which simultaneously affect fouling deposition and
460 removal mechanisms. Moreover, differences in fuel types can lead to changes in
461 exhaust composition, thereby influencing fouling morphology [50].

462 This section discusses the influence of key variables on fouling morphology.
463 Through the above analysis, we further recognise that multiple system variables jointly
464 affect fouling morphology, as shown in Figure 13. This is because system variables are
465 the original factors triggering fouling mechanisms. By controlling system variables, we
466 can alter different types of mechanisms and their intensities, including but not limited
467 to deposition mechanisms (such as particulate matter deposition and hydrocarbon
468 deposition), removal mechanisms, and the relative contributions of various sub-
469 mechanisms. Therefore, an in-depth study of the relationship between system
470 variables and fouling morphology helps us to comprehensively understand complex
471 fouling mechanisms.



472

473 **Figure 13.** Overview of system variables affecting EGR coolers fouling morphology

474 **6. The morphology–property correlation**

475 **Table 2** provides a concise summary of the 18 past studies that reported the
 476 relationship between fouling morphology and properties. The properties covered
 477 include density, thermal conductivity/thermal resistance, mechanical properties,
 478 water stability, crushing strength and stiffness, removal /shear stability, thermal
 479 stability, and adhesion force. Here, we categorise these into four groups: density,
 480 thermal properties, mechanical properties, and stability properties, which are
 481 elaborated upon in detail below.

482 **Table 2**
 483 Summary of the investigation on the correlation between morphology and property
 484 for exhaust gas recirculation coolers fouling

Reference	Year	Fouling morphology category	Fouling property
Lance et al. [62]	2009	Porosity	Density; Thermal conductivity
Teng and Barnard [63]	2009	Size of pores; Porosity; Layering state	Thermal conductivity / thermal resistance; Mechanical properties
Teng and Barnard [64]	2010	Size of pores; Porosity; Layering state	Density; Thermal conductivity; Mechanical properties; Water stability
Lance et al. [65]	2010	Not reported	Water stability
Lance et al. [17]	2010	Connection way of particulate matters	Density
Lance et al. [66]	2011	Porosity/compactness	Density; Thermal conductivity; Crushing strength and stiffness
Abarham et al. [22]	2012	Fragmentation	Remove stability
Abarham et al. [23]	2013	Fragmentation	Remove stability
Furuhata et al. [30]	2014	Fragmentation	Remove stability
Salvi et al. [49]	2014	Compactness	Thermal stability
Han et al., [13]	2015	Fragmentation	Remove stability
Matsudaira et al. [52]	2017	Fragmentation	Remove stability
Lance et al. [54]	2018	Porosity	Density
Razmavar and	2019	Compactness	Adhesion force

Malayeri [67]			
Paz et al. [29]	2021	Porosity; Size of particulate matter; Wetness	Density
Cook et al. [55]	2022	Structure of pores	Thermal stability
Han et al. [39]	2023	Size and way of particulate matter connection	Thermal conductivity
Vence et al. [40]	2023	Wetness	Density

485 6.1. Density

486 The morphology of fouling is closely related to fundamental material properties
 487 such as density, colour, and phase state. Colour and phase state, being both
 488 morphological aspects and basic material properties, have been discussed previously
 489 and will not be elaborated upon here. This section focuses on the correlation between
 490 morphology and density.

491 Lance et al.'s research indicates that the average density of fouling is
 492 approximately 0.035 g/cm³, with a porosity as high as 98% [62]. In a subsequent study,
 493 they further discovered that the low density is primarily due to the connection method
 494 between sub-units (particulate matters), which occurs through narrow bridges of only
 495 about 15 nm [17]. Vence et al.'s research found that fouling with more wet
 496 components also has a higher density [40]. Similarly, Lance et al. observed that
 497 hydrocarbon condensation encapsulating particulate matter can form fouling with
 498 fewer pores and greater density [54]. Paz et al. further quantified the density of fouling
 499 formed under different degrees of hydrocarbon condensation, providing a more
 500 comprehensive understanding of the relationship between condensation and fouling
 501 density [29]. Teng and Barnard proposed a three-layer substructure model for fouling,
 502 including a base layer, intermediate layer, and surface layer. The surface layer is highly
 503 porous with low density and thermal conductivity; the base layer has low porosity,
 504 high density, and the best thermal conductivity; the intermediate layer's pore
 505 morphology, density, and thermal conductivity are between the two [64].

506 Overall, morphological characteristics such as wetness, densification, and sub-
 507 unit connection methods are key factors influencing fouling density. This relationship
 508 between morphology and density not only enhances our understanding of fouling
 509 structure but also provides valuable insights for predicting and controlling fouling
 510 properties in practical applications.

511 6.2. Thermal property

512 Thermal conductivity is a core parameter of thermal properties. Lance et al.
 513 determined that the average thermal conductivity of fouling is approximately 0.041
 514 W/(mK), significantly lower than that of metallic materials (e.g., 304 stainless steel at

515 14.7 W/(mK)) and closer to that of air (0.025 W/(mK)) and certain insulating materials
516 (such as glass fibre and R-12 expanded and extruded polystyrene). This is primarily
517 attributed to the high porosity of fouling [62]. A report by Lance et al. also indicated
518 that thermal conductivity is mainly controlled by fouling density [66]. Teng and
519 Barnard further developed a negative correlation curve between thermal conductivity
520 and porosity based on literature and experimental results, demonstrating that higher
521 porosity corresponds to lower thermal conductivity [64].

522 Teng and Barnard proposed a three-layer substructure model of fouling,
523 suggesting that particle size and deposition patterns influence the morphology of the
524 deposition layer. The thermal conductivity of the corresponding fouling layers
525 decreases progressively (thermal resistance increases), from inner layers with micro
526 pores (< 10 nm) to a randomly-packed intermediate layer with meso pores (10-50 nm),
527 and finally to a loose surface layer with macro pores (> 50 nm) [63]. Han et al. posit
528 that in scenarios involving hydrocarbon condensation, the enlargement of particulate
529 matter within fouling may construct a more robust heat transfer framework, thereby
530 enhancing overall thermal conductivity [39]. Generally, the morphological
531 characteristics of fouling, particularly porosity and particle size, directly influence its
532 thermal conductivity. Moreover, as thermal conductivity is closely related to density
533 [64], morphological features affecting density also indirectly impact thermal
534 conductivity.

535 **6.3. Mechanical property**

536 The relationship between the morphology and mechanical properties of the
537 fouling may lie in their layered structure: the base layer, formed by nanoparticles
538 through van der Waals forces and interactions with the metal surface, exhibits
539 relatively high density; the intermediate layer has a moderate density; while the
540 surface layer, composed of particle clusters connected by mechanical interlock,
541 features high porosity and low density. This stratified structure highlights the intrinsic
542 correlation between fouling morphology and mechanical properties [63, 64]. Lance et
543 al. were the first to report the use of Load-Displacement Curves to characterise the
544 crushing strength and stiffness of fouling, and they found that the load for Light-Duty
545 fouling could approach approximately 1 kPa [66]. However, no results of Load-
546 Displacement Curves for other types or forms of fouling were provided for comparison.

547 Razmavar and Malayeri discovered that fouling formed on treated coated
548 surfaces was more porous than that on untreated surfaces, as evidenced by the
549 surface adhesion of the two types of fouling. The results revealed that the adhesion of
550 fouling to the substrate stainless steel was approximately three times greater than that
551 to the coated surface, indicating that fouling on coated surfaces exhibits weaker
552 adhesion and is consequently easier to remove [67]. This finding elucidates the close
553 relationship between the compactness of fouling morphology and its adhesiveness.
554 The results provide valuable insights for developing novel cleaning methods,
555 potentially mitigating the adverse consequences of fouling.

556 **6.4. Stability property**

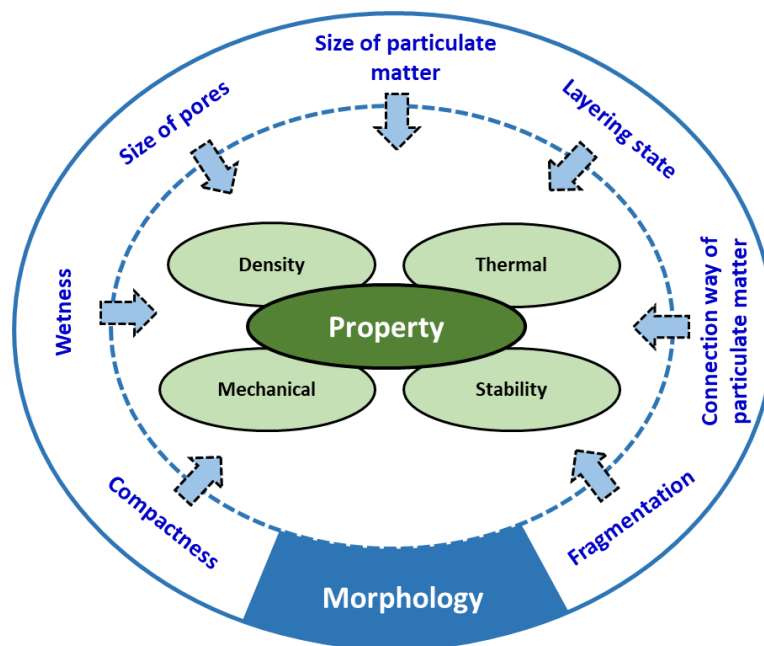
557 Research indicates a strong correlation between the thermal stability of fouling
558 and its morphology. Cook et al. observed that raw fouling softens at 100°C and melts
559 at 150°C, whereas an extracted soluble substance remained stable even at 300°C. They
560 postulated that this enhanced thermal stability might result from the soluble
561 substance obstructing the fouling's pores, thereby retarding oxidation [55]. Salvi et al.
562 noted that fouling exhibited fragile dendritic features before high-temperature baking,
563 but after one baking cycle, it displayed more agglomerated characteristics, with
564 reduced area ratio, smoother surface, and decreased thickness. A second baking cycle
565 further reduced the fouling thickness. They attributed this to the collapse of porous
566 fouling structures due to higher kinetic energy during heating [49]. Thermal stability
567 typically results from the combined effects of composition and morphology. Although
568 quantitative studies distinguishing the specific contributions of morphology and
569 composition to thermal stability are currently lacking, these findings clearly
570 demonstrate the close relationship between fouling morphology and thermal stability.
571 The porous structure of fouling influences its thermal stability, while thermal
572 treatment alters the fouling morphology, creating a cycle of mutual influence.

573 Moreover, the morphology of fouling can change through hydration [64] or water
574 immersion and drying [65]. These processes are complex but are generally related to
575 the susceptibility of the porous fouling structure to collapse under liquid-phase forces
576 and thermal stresses.

577 In addition to the aforementioned thermal and water stability, the evaluation of
578 the remove/shear stability, which reflects the ease of removal of fouling by airflow
579 shear forces, is also related to the morphology of the fouling. Han et al., in their
580 conceptual model incorporating three removal mechanisms, pointed out that one
581 scenario involves fouling being removed through airflow shear forces due to mud-
582 cracking [13]. Furuhashi et al. [30], Matsudaira et al. [52] and Abarham et al. [22, 23]
583 observed how fouling was progressively removed in areas with a higher degree of
584 fragmentation, as detailed in Section 4.1. Interestingly, experimental findings by Lance
585 et al. reported that when fouling is stripped off, the fracture surface is within the
586 fouling itself rather than at the fouling-metal interface, which may be associated with
587 the presence of large voids within the layers [66]. Taken together, the degree of surface
588 fragmentation and the presence of large voids within the fouling may be related to its
589 stability against shear forces from exhaust airflow.

590 In conclusion, as shown in **Figure 14**, fouling morphology significantly affects its
591 density, thermal, mechanical, and stability properties, which in turn directly determine
592 cooler performance. For heat exchangers, the thermal conductivity of fouling is crucial
593 and is primarily dependent on morphological characteristics such as porosity,
594 wettability, and the scale of the heat transfer skeleton. Additionally, pressure drop,
595 another critical parameter for evaluating heat exchanger performance, is mainly
596 influenced by fouling thickness and surface topography. Fouling thickness results from
597 the interplay between deposition and removal mechanisms, with removal

598 effectiveness closely related to surface mechanical properties, which are influenced by
 599 fouling compactness. Despite the complex interrelationships between morphology
 600 and properties, in-depth analysis reveals that fouling morphology may be the more
 601 fundamental factor. It not only affects fouling thickness and surface topography but
 602 also further influences gas flow patterns, ultimately leading to negative consequences
 603 on pressure drop. Therefore, a deep understanding and control of fouling morphology
 604 are crucial for optimising heat exchanger performance.



605
 606 **Figure 14.** Overview of fouling morphology affecting fouling properties in EGR coolers

607 7. Challenges and opportunities

608 Throughout the review and analysis of EGR cooler fouling morphology, several
 609 limitations and challenges have been identified, which can serve as directions for
 610 future endeavours:

611 (1). Organic integration of multi-scale characterisation

612 Most studies typically focus on only one or two of the four scales (macro, meso,
 613 micro, and nano), with few encompassing all four. This limitation leads to an
 614 incomplete understanding of fouling morphology. However, a comprehensive
 615 and systematic understanding of the subject requires in-depth knowledge of
 616 each level, its sub-units, and their connections. Therefore, organic multi-scale or
 617 even full-scale morphological characterisation is a research direction worth
 618 exploring.

619 (2). Developing more quantitative morphological categories and indicators

620 Morphology covers three dimensions: shape, size, and structure, encompassing
 621 a series of characterisation categories, each of which can be realised through

622 different characterisation indicators, resulting in considerable depth and rich
623 hierarchical structure. However, based on the analysis of past literature, we
624 found that morphological characterisation in most studies remains qualitative,
625 with quantitative characterisation being relatively rare. This is evident in the
626 literature, where textual descriptions predominate over precise data
627 presentation. This *status quo* not only hinders the dissemination and horizontal
628 comparison of scientific knowledge but also makes it difficult to clearly and
629 directly convey characterisation results to peers or readers. Therefore,
630 developing more quantitative morphological categories and indicators is of great
631 significance. For instance, some fouling has been confirmed to have fractal
632 characteristics [64, 68], yet verbal qualitative descriptions of them are often
633 inadequate. Parameters from fractal science (such as fractal dimension, self-
634 similarity dimension, etc.) could be employed for quantitative characterisation.

635 **(3). Refining fouling nomenclature and taxonomy based on morphological science**

636 Some disciplines have utilised morphology to complete the classification,
637 naming, and mapping of research objects, which provides a common
638 communication framework for the industry, such as [69-72]. However, in the EGR
639 cooler fouling field, although mechanism-based classification and naming exist,
640 this classification remains rudimentary. Morphology-based classification has
641 only been addressed in a few studies and has not yet formed an industry
642 consensus, remaining largely a blank field. Therefore, drawing on morphological
643 classification experiences from other fields, establishing typical fouling
644 morphologies, naming them, and creating atlases will be of significant value for
645 standardisation in the fouling field.

646 **(4). Refinement of fouling morphology evolution patterns over the full life cycle**

647 Generation, growth, removal, stabilisation, and ageing are typically considered
648 the complete lifecycle of fouling. Although previous studies have confirmed that
649 morphology can provide intuitive visual evidence for the generation, growth,
650 removal, and stabilisation processes of fouling, visual evidence for the ageing
651 process is still lacking. Moreover, most studies focus on only one or two of these
652 five classic stages, with varying time scales across different research projects,
653 which may be short-term, medium-term, or limited to a specific stage. To date,
654 no study has provided continuous evidence documenting the entire lifecycle
655 evolution of fouling. Therefore, it is necessary to conduct in-depth research and
656 enrich our understanding of the morphological evolution patterns of fouling
657 throughout its entire lifecycle.

658 **8. Conclusion**

659 This comprehensive study on EGR cooler fouling morphology introduces a
660 systematic overview that encompasses characterisation, spatiotemporal distribution
661 nature, variable-morphology correlation, morphology-property correlation, and

662 challenges and opportunities. The main findings and contributions are as follows:

663 (1). A characterisation framework for EGR cooler fouling morphology is developed,
664 facilitating enhanced communication and comparative analysis among studies.

665 (2). Morphology plays a vital role in revealing the evolution process of fouling,
666 including its generation and growth, and provides direct and explicit evidence for
667 understanding fouling deposition and removal mechanisms. Meanwhile, it serves
668 as a key perspective for understanding the intrinsic relationships between system
669 variables, fouling, and properties.

670 (3). Future research on morphology could focus on the integration of multi-scale
671 characterisation, the refinement of quantitative morphological categories and
672 indicators, the development of nomenclature and taxonomy, and a
673 comprehensive understanding of fouling evolution patterns.

674 This systematic review of EGR cooler fouling morphology deepens understanding
675 of fouling generation and mitigation mechanisms and provides a crucial framework for
676 advancing fouling morphology science.

677 **Credit authorship contribution statement**

678 **Yipeng Yao**: Conceptualization, Methodology, Writing – review & editing,
679 Visualization, Supervision, Project administration. **Zhiqiang Han**: Conceptualization,
680 Methodology, Validation, Investigation, Writing – review & editing. **Liping Luo**:
681 Software, Formal analysis, Investigation, Visualisation. **Hai Du**: Writing – review &
682 editing, Visualisation. **Wei Tian**: Formal analysis, Investigation, Visualisation. **Xueshun**
683 **Wu**: Software, Writing – review & editing. **Zinong Zuo**: Writing – original draft. **Marie-**
684 **Eve Duprez**: Writing – review & editing. **Guy De Weireld**: Writing – review & editing,
685 Supervision.

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693 **Data Availability**

694 Data will be made available on request.

695 **Declaration of generative AI and AI-assisted technologies in the** 696 **writing process**

697 During the preparation of this work, Yipeng YAO used ChatGPT to improve the

698 readability and language of the manuscript. After using this service, the Yipeng YAO
699 reviewed and edited the content as needed and take(s) full responsibility for the
700 content of the published article.

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