

Ground demonstration of the use of *Limnospira indica* for air revitalization in a bioregenerative life support system setup: effect of non-nitrified urine derived nitrogen sources.

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Author contribution statement

NS conducted all the experiments the data. NS and LP worked on the Photosim 2.0 model. BL and OG worked on the control law. CGD, CL, BL and RW supervised the study. NS, BL and RW wrote the manuscript. All authors contributed equally to data analysis, interpretation and

Keywords

Regenerative life support system, Crewed space exploration, *Limnospira indica*, oxygen production, Nitrogen and Carbon waste recycle, MELiSSA Loop

Abstract

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Long-duration human space-missions require considerable amounts of water, oxygen and nutritious biomass. Additionally, the space-vehicles must be well-equipped to deal with metabolic human-waste. It is therefore important to develop life-support system which make these missions self-sufficient in terms of water, food and oxygen production as well as waste management. One such solution is the employment of regenerative life-support systems that use biological and chemical/physical processes to recycle crew-waste, revitalize air and produce water and food. Photosynthetic cyanobacteria *Limnospira* could play a significant role meeting these objectives. *Limnospira* can metabolize CO₂ and nitrogen-rich human-waste to produce oxygen and edible biomass. So far, life-support system studies have mainly focused on using chemical/physical methods to recycle water, degrade human-waste and recycle CO₂ to oxygen. Nowadays, additional microbial processes are considered, such as nitrification of urea-ammonium rich human-waste and then use the nitrate for cyanobacterial cultivation and air-vitalization. This cascade of multiple processes tends to increase the complexity of the life-support systems. The possibility to use non-nitrified urine for *Limnospira* cultivation can partially solve these issues. Our previous studies have shown that it is possible to cultivate *Limnospira* with urea and ammonium; the prominent nitrogen-forms present in non-nitrified urine. In this study, we investigated the possibility to cultivate *Limnospira* with the different nitrogen-forms present in non-nitrified urine and also evaluated their effect on the oxygen production capacity of *Limnospira*.

For this 35-days long study we worked on a simplified version of European Space Agency's MELiSSA. During this ground-demonstration study, we monitored the effect of urea and ammonium (vs nitrate) on the oxygen production capacity of *Limnospira*. A deterministic control law, developed and validated on the basis of a stochastic light-transfer model, modulated (increase/decrease) the incident light on the photobioreactor (with *Limnospira*) to control oxygen levels in the closed loop. The CO₂ from mouse compartment was recycled as carbon-source for *Limnospira*. We observed that while the system could meet the desired oxygen levels of 20.3% under nitrate and urea regime, it could only reach a maximum O₂ level of 19.5% under ammonium regime.

Contribution to the field

In this manuscript we have demonstrated a regenerative life support system setup which is a modified prototype of European Space Agency's MELiSSA. Through this study we demonstrated the possibility to (a) revitalize air, (b) simulate and control the oxygen levels in the closed loop by modulating the incident light intensity in the photobioreactor, for photosynthetic cultivation of *Limnospira indica* and (c) use urea and ammonium (present in human metabolic waste) as nitrogen sources for photosynthetic cultivation of cyanobacteria *Limnospira indica*. Briefly, for this study, an eight weeks old mouse (housed in a closed animal cage) was the consumer and *Limnospira indica* (cultivated in a photobioreactor) was used as the producer. The producer (*Limnospira indica*) and consumer (mouse) compartments were connected through a closed gas loop to enable gas exchange. We also monitored the effect of alternative nitrogen sources (nitrate, urea and ammonium) on the oxygen production capacity of *Limnospira indica*. A radiant-light-transfer model was used to control the oxygen production in photobioreactor at defined levels (as per respiratory needs of mouse). Highlights • Regenerative life support system for long-term manned space missions • Coupling of photobioreactor and mouse cage in closed gas loop • Air revitalization using cyanobacteria cultivated in photobioreactor • Transient feeding of three nitrogen sources (ammonium, urea and nitrate) in photobioreactor • Controlled oxygen production using light-transfer model based control law

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In review

Ground demonstration of the use of *Limnospira indica* for air revitalization in a bioregenerative life support system setup: effect of non-nitrified urine derived nitrogen sources.

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Abstract

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meeting these objectives. *Limnospira* can metabolize CO₂ and nitrogen-rich human-waste to produce oxygen and edible biomass.

So far, life-support system studies have mainly focused on using chemical/physical methods to recycle water, degrade human-waste and recycle CO₂ to oxygen. Nowadays, additional microbial processes are considered, such as nitrification of urea-ammonium rich human-waste and then use the nitrate for cyanobacterial cultivation and air-vitalization. This cascade of multiple processes tends to increase the complexity of the life-support systems. The possibility to use non-nitrified urine for *Limnospira* cultivation can partially solve these issues. Our previous studies have shown that it is possible to cultivate *Limnospira* with urea and ammonium; the prominent nitrogen-forms present in non-nitrified urine. In this study, we investigated the possibility to cultivate *Limnospira* with the different nitrogen-forms present in non-nitrified urine and also evaluated their effect on the oxygen production capacity of *Limnospira*.

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1. Introduction

Current space missions mainly rely on physical/chemical processes for water recycling and air revitalization. Food and other consumables are periodically resupplied from Earth. However, constraints associated with payload, launch technologies and distance would drastically restrict such resupplies for future space missions to distant planets like Mars. Depending on the orbital distance and synodic period, one way trip to Mars can take around 300 days (Portree, 2001). An average person needs 15-20 kg of essential supplies per day in terms of O₂, food, drinking water and hygiene water (Farges et al., 2008; Anderson et al., 2015). This effectively means that around 90-120 ton of essential supplies would be needed for a crew of 6.0 people for a 1000 day return-mission to Mars. Lowering this payload will be an asset for the long-duration human space missions. Though certain chemical methods are currently used to recycle water and O₂ onboard space flights, food and other essential supplies have to be periodically resupplied from Earth. Furthermore, provisions must be made to safely deal with human metabolic waste and efforts must be made to reduce the dependence on physical and chemical waste-treatment processes. It is therefore important to look for practical alternatives to increase the self-sustainability of long-term human space missions in terms of food production, air-revitalization, waste management and water recycling.

Several international space agencies and research organizations have been investigating the possibility of cultivating photosynthetic species (microalgae, cyanobacterial and plants) on board space-flights for food production, air revitalization, waste management and water recycling (Karel, 1982; MacElroy and Brecht, 1984; MacElroy et al., 1987; Mergeay et al., 1988; Gitelson et al., 1989; Lasseur et al., 1996; Kibe et al., 1997; Farges et al., 2008; Lasseur et al., 2010; Hader, 2020; Helisch et al., 2020; Zhang et al., 2020).

Erstwhile USSR (now Russia) were one of the pioneers who worked on microalgae based regenerative life support systems (LSS). (Gitelson et al., 1989). Their LSS mainly had four

compartments: one for algae (*Chlorella* sp.), one for crew and two for plants (wheat and vegetables). The first test on this system (1972) mainly focused on water and CO₂ recycling and lasted for 180 days. For this study food (for human consumption) was sourced externally and no provision was made for metabolic waste treatment within the LSS.

National Aeronautics and Space Administration (NASA), USA started to work on their microalgae based regenerative LSS under the project name: Controlled Ecological Life Support System (CELSS) (MacElroy and Bredt, 1984; Averner, 1990). The CELSS system was conceived with the aim of producing edible biomass from plants and microalgae *Chlorella* sp. The system also aimed to purify water, revitalize air and recycle waste under closed-loop conditions (MacElroy et al., 1987). However, the CELSS project was soon discarded, and NASA decided to focus their life-support research on plant compartment under the project name VEGGIE (NASA Techport, 2017; Massa et al., 2018; Monje et al., 2020). Now a days, NASA is exploring the possibility of using their VEGGIE compartment for the co-cultivation of plants and the microalgae *C. reinhardtii*. NASA researchers have been recently working on the development of bioprocesses and cultivation systems that can protect the microalgae from the inhibitory effects of microgravity and harmful radiations (Monje et al., 2020). Zhang et al., (2020) used molecular techniques to design tissue bag-based cultivation systems for the cultivation UV-resistant mutants of microalgae *C. reinhardtii* in VEGGIE growth chamber.

Japanese Aerospace Exploration Agency (JAXA), is also investigating the possibility of including photosynthetic microalgae (*Chlamydomonas* sp.) for waste recycling and production of food and O₂ production under the umbrella of their regenerative LSS project: Closed Ecology Experiment Facility (CEEF) (Kibe et al., 1997; Kage et al., 2011 and 2013).

European Space Agency (ESA), through its MELiSSA (Micro Ecological Life Support System Alternative) project, is currently involved in the development of a self-sustainable regenerative

LSS project. Structurally, MELiSSA is inspired from the function of natural lake-ecosystem. The five compartments of the MELiSSA loop (see Fig.1A, De Meur, 2017) mimic the various functions of the lake-ecosystem. Briefly, the first compartment (CI), which is inhabited by consortia of thermophilic bacteria, degrades the complex human waste and inedible plant biomass to volatile fatty acids (VFAs), carbon dioxide (CO_2) and ammonium (NH_4^+). These VFAs are then further oxidized to CO_2 and NH_4^+ in the second compartment (CII) inhabited by purple photosynthetic bacteria *Rhodospirillum rubrum*. The nitrifying bacteria in the third compartment (CIII) then oxidize NH_4^+ to nitrate (NO_3^-), which is then used as the nitrogen (N) source along with CO_2 for cultivation of cyanobacteria *Limnospira indica* (formerly *Arthrospira* sp. PCC 8005) and plants in the producer compartments CIVa and CIVb, respectively. The O_2 , water and edible biomass produced in the producer compartments are consumed by the crew in the consumer compartment.

MELiSSA scientists and engineers have conducted several studies in the past to investigate the efficiency and performance of interconnectivity of two or more compartments under closed loop conditions (Demey et al., 2000; Alemany et al., 2019). These terrestrial studies, also known as ground demonstration (GD) studies, were based on the premise that the nitrification compartment (CIII) will convert urea and NH_4^+ to NO_3^- , which will then be used for cyanobacterial cultivation in the producer compartment. However, the sub-optimal working of the nitrification compartment, could result in incomplete nitrification. This in turn would result in the transfer of urea and NH_4^+ rich waste streams into compartment CIVa. Therefore, it is necessary to evaluate the possibility of using partially nitrified or even non-nitrified urine (urea and NH_4^+ rich) for cyanobacterial cultivation and understand their effect on the biomass yield, biomass composition/quality (biochemistry) and O_2 productivity.

Several studies have been conducted in the past to evaluate the effect of different N-sources (NH_4^+ , NO_3^- , NO_2^- and urea), their feeding mode (batch, fed batch or continuous) and

concentrations; on the overall yield and quality/composition of *Limnospira* biomass (Sassano et al., 2004; Avila-Leon et al., 2012; Markou et al., 2015; Deschoenmaecker et al., 2017; Sachdeva et al., 2018a and 2018b). These studies have shown that compared to NO_3^- , urea enhances the protein and pigment content in the *Limnospira* biomass (Sassano et al., 2004; Avila-Leon et al., 2012 and Sachdeva et al., 2018b). In contrast, NH_4^+ feeding has been reported to increase the lipid and exopolysaccharide content in the *Limnospira* biomass, while decreasing biomass yield (Markou et al., 2014; Sassano et al., 2010; Deschoenmaecker et al., 2017; Sachdeva et al., 2018a and 2018b). These previous studies have hence established that (1) it is possible to cultivate *Limnospira* with alternative N-sources and (2) changing the N-concentration, N-source type and feeding mode could modify the biochemical composition and biomass yield of *Limnospira*.

However, none of these studies had evaluated the effect of the alternative N-sources on the O_2 production and air revitalization potential of *Limnospira*. In order to fill in this gap, we conducted the present GD study wherein we evaluated the O_2 production capacity and air- revitalization characteristics of *Limnospira* under closed loop conditions of MELiSSA LSS. For this study, *Limnospira* was cultivated in a photobioreactor (PBR)/ producer compartment and the mouse, housed in a closed animal cage, was used as the consumer. The producer compartment and the consumer compartment were connected through a closed and airtight gas loop. The complete setup (breadboard) is described under Fig.1B.

The O_2 produced in producer compartment was used for air-revitalization in consumer compartment and the CO_2 from consumer compartment was used as the carbon source for cyanobacterial cultivation in producer compartment. A stochastic light-transfer based model developed in our previous study (Sachdeva et al., 2018a) was used to define a deterministic control law which controlled the O_2 levels in the producer compartment by modulating the

incident light flux on the PBR. As part of study protocol (Fig.2) the N-sources in the cyanobacterial feeding medium were changed between NO_3^- , NH_4^+ and urea.

The preliminary data obtained through this 35 days long GD study clearly demonstrated that (1) it is possible to couple the producer compartment and consumer compartment under the closed loop conditions for air-revitalization and (2) it is possible to use different N-forms (present in untreated urine) for cyanobacterial cultivation and O_2 production.

2. Materials and Methods

2.1 System Setup: Connections between the compartments and data monitoring

The basic layout of the GD breadboard is represented in Fig.1B. The producer compartment and the consumer compartment were connected via a closed gas loop. The EU directive 2010/63/EU mandates a minimum of 10 air exchanges per hour for an animal compartment. Accordingly, minimum air flow rate of 55.0 L/hr was required for this 11.5 L cage. On the other hand, the gas flow rate in the PBR had to be maintained below 3.0 L/hr to avoid cell shearing and culture foaming. This PBR flow rate was decided as per the results of our preliminary tests (data not shown). To accommodate two separate gas flow rates, the gas loop was bifurcated into primary and secondary loop.

The primary loop mainly consisted of the consumer compartment, pressure monitor (PI), flow transmitter (FT) and flow controller (FC). The gas flow rate in primary loop was maintained at 55 L/hr using an external pump. The presence of activated charcoal trap and 0.2 microns filter prevented the transmission of microbes and ammonia from the consumer compartment to the gas loop (in the primary loop). The consumer compartment outlet was connected to a sensor line, which continuously monitored the O_2 levels in molar percentage. This sensor line consisted of a dehumidifying bottle, flow controller and an O_2 sensor. The O_2 sensor (9212-

5AD, Analox Sensor Technology, USA) used for this study was found to be sensitive to high gas flow rates. Therefore, the gas flow rate in the sensor line was controlled at 100 mL/min.

A calibration line was also provided along the sensor line to ensure periodic calibration of O₂ sensor without opening the gas loop. Two gas mixes (1) 99.99% N₂ (for zero) and (2) 21% O₂, 1.0% CO₂ and 78% N₂ (similar to atmospheric O₂ composition). A safety line (safety valve) was also connected to the consumer compartment outlet. This safety valve ensured opening of the closed gas loop in case the O₂ levels in the consumer compartment increased or decreased beyond the safety range (17.5% to 24% O₂). The other end of this safety line was connected to compressed air cylinder that ensured air supply to consumer compartment in the case of system failure.

The secondary loop consisted of producer compartment (PBR and lightening unit). Manual valves, flow transmitter and low controller were provided throughout the secondary loop to control and monitor the gas flow. The control law (see below) modulated the incident light flux of this lightening system attached to the PBR. The outlet of PBR was connected to a dehumidifying bottle, PI and 0.2 microns filter.

2.2. Cyanobacterial Culture and Photobioreactor Setup

The stock culture of *Limnospira indica* (previously *Arthrospira* sp. PCC 8005) strain was maintained under axenic conditions in Cogne-Modified Zarrouk Medium (Cogne et al., 2003) with 8.5 mM NaNO₃ as the N-source (Sachdeva et al. 2018b). For the GD test, *Limnospira indica* was cultivated in a 2.0-L double-jacked cylindrical PBR (Biostat®, Sartorius AG, Germany). PBR was radially illuminated using 14 cool-white light bulbs (4000K, 12V, Philips) and the culture was mixed at 150 rpm with a Rushton turbine. The PBR working volume, dilution rate and incident light flux were selected on the basis of the respiratory requirements of 21.4 gm mouse used as the consumer for this study (see following section). The details of criteria used to define these working parameters have been defined in Demey et al. (2000) and

will not be discussed here. This setup (PBR culture vessel and lightening unit) was termed as the producer compartment. *Limnospira indica* was cultivated at controlled temperature (36 °C) and pH (8.5) in carbonate and bicarbonate free Zarrouk medium. CO₂ from consumer compartment served as carbon source for *Limnospira* pH was controlled using 0.5 N HCl and 1.0 N NaOH. Based on the study protocol (Fig.2), the N-source (8.5 mM each) in feeding medium were changed between NaNO₃, NH₄Cl and urea. pH of 8.5 was chosen to avoid loss of NH₄⁺ as NH₃ (Sachdeva et al., 2018a). Under the current cultivation conditions (pH, dilution rate, biomass concentrations) CO₂/ carbon limitation was not foreseen. This simulation is based on the results of a previous MELiSSA LSS study (Demey et al., 2000) and hence is not discussed here.

Prior to the start of GD study, the PBR was maintained under batch mode (with 8.5 mM NaNO₃) for five days [Day (-1) to Day (-5)]. Once the culture reached an optical density (at 750 nm) of 1.5 ±0.2 the continuous feeding was started and this day was termed as Day (D) 1 of the GD study. The dilution/feeding rate for the continuous feeding was fixed at 0.2 (volume) per day to maintain culture OD at 1.5 ±0.2. This dilution rate and reference OD were adopted on the basis of the results of our previous study (Sachdeva et al., 2018a) used to define the control law used for this GD study (see following sections). Based on this dilution rate, one residence time was defined at 5 days. The mouse was put in the consumer compartment on D1 of GD study.

Nitrate regime was used as the control for this study and accordingly the PBR was maintained under continuous feeding of 8.5 mM NaNO₃ for five days (D1-D5). This period is termed as the NO₃⁻ regime.

First transition to 8.5 mM NH₄Cl was performed on D6. The first five days (D6-D10) of NO₃⁻-to-NH₄⁺ transition, were excluded from NH₄⁺ regime (Fig.S1) to avoid quantitative bias (see

discussion section for more details). Consequently, D11-D20 were be designated under NH_4^+ regime. Similarly, for urea regime, the first five days of NH_4^+ -to-urea transition (D21-D25) were excluded from quantitative analysis, and D26-D35 were considered under urea regime.

2.3 Test animal and Consumer Compartment

An eight-weeks old, C57BL/6J male mouse was used as the consumer for this GD study. The research work (on mouse) for this study was conducted in accordance with the ethical committee agreement LA 1500024, (Project Code: RI-10-01) dated 28th August 2018.

The mouse weighed 21.2 gm at the beginning of study. The mouse was housed in a stainless-steel cage (consumer compartment), which had a total volume of 11.5 liters. The design of the cage was compliant with the EU Directive 2010/63/EU.

Internally the cage was separated into two parts by a perforated slide. While the mouse occupied the upper compartment, the lower compartment was layered with dried wooden shavings. The perforated slide between the upper and lower compartments enabled the mouse urine and feces to fall on the lower compartment (containing the wooden shaving), to facilitate moisture absorption and maintain proper sanitation in the upper compartment occupied by the mouse. This enabled a smooth non-stop running of the GD study for 35 days without the need to open the cage for cleaning and sanitization. The exterior of the cage had an inlet and outlet for gas exchange.

Food and water requirements of mouse were calculated as per its weight before the start of the experiment. An eight-weeks old C57BL/6J male mouse normally requires 8-10 ml water and 3.5-4.5 gm of food per day (Bachmanov et al., 2002). A mouse requires 3.3 gm $\text{O}_2/\text{kg}\cdot\text{hr}$ (vs 5144 gm $\text{O}_2/\text{kg}\cdot\text{hr}$ for an average human; Demey et al., 2000). Food and water were provided *ad libitum*. A 500 mL drinking water bottle was connected to the cage via a drinking nipple. Pre-weighed food pellets were provided through the food chute, located on the side of the cage.

An automated light switch in the cage ensured that the mouse was exposed to a 12:12 hour dark-light cycle. One cool-fluorescent light bulb (3000K, 36V, GE) was used to illuminate the consumer compartment. This selection was made on the basis of animal study protocol directives. The CFL light bulb used in animal housing had no direct contact or exposure to the PBR unit used for cyanobacterial cultivation.

Prior to the start of GD study, the mouse was allowed to acclimatize to its new environment. For this acclimatization period, the mouse was housed in the cage for eight hours per day for a total period of 5.0 days. During this acclimatization period, we monitored the mouse for its behavioral changes and response to pump noise, temperature, new feeding and drinking mode, etc. No data was collected during this period.

The gender of the mouse was not foreseen to affect the study outcome. Only one mouse was used for this study mainly as per the EU Directive 2010/63/EU and clauses of the ethical committee agreement used to conduct this animal study.

2.4 Control law and safety system

The control law used for this study was trained and validated in accordance with the updated light-transfer-model (Photosim 2.0 model hereafter), reported by Sachdeva et al. (2018a). Photosim 2.0 model and its prediction parameters had already been tested and validated in the context of the cultivation parameters used for this GD study and thus would not be discussed here.

The control law also ensured safety within the closed loop in case of system failure. It controlled the opening/ closing of the safety valve in accordance with the defined safety parameters. The safety parameters were defined at $< 17.5\%$ and $> 24\%$ for O_2 . In a scenario when the O_2 levels in the loop were higher or lower than these safety limits, the control law

automatically opened the safety valve attached to the consumer compartment and ensured the supply of compressed air to the animal compartment to avoid animal distress.

2.5 Data collection and analysis

The Arduino program recorded O₂ in molar percentage (%O₂) and incident light flux (W/m²) once every 5.0 seconds. For the graphical representation, each data point on the graph is reported as the average of 15 minutes. Paired T-test was used to calculate *p-value*.

3. Results

3.1 Nitrate Regime

A total of 553 readings (for light flux and O₂ level) were recorded under the NO₃⁻ regime (D1-D5). Overall, the system applied an average light flux of 136W/m² to maintain average O₂ levels of 20.3% over the five days (D1-D5) of NO₃⁻ regime (Fig.3 and Fig.4). Out of these 553 recorded readings, only 34 readings had O₂ levels less than 20%. The minimum O₂ level of 19.9% was observed for only 3 (recorded) readings during the five days of NO₃⁻ regime, where the system was seen to reach the illumination limit (in terms of light flux) of 147.1W/m². The system reached the highest O₂ level of 21.1% under the NO₃⁻ regime.

3.2 Ammonium Regime

The first transition to NH₄⁺ was performed on D6 of GD (Fig.2). Since the system was replacing residual NO₃⁻ with NH₄⁺, the first five days (D6-D10) of NO₃⁻-to-NH₄⁺ transition were not considered under NH₄⁺ regime. Consequently, D11-D20 were considered under NH₄⁺ regime (Fig.3 and Fig.5).

A total of 1155 readings (for light flux and O₂ level) were recorded under NH₄⁺ regime. The system was found to work under illumination limit (147.1W/m² light flux) on 82.9% of the recordings (958 out of 1155 recordings) and could reach the O₂ setpoint (20.3% or higher) for only 9% of these recorded values. Overall, the system maintained an average O₂ level of 19.5%

during the ten days of NH_4^+ regime, under an average light flux of 146.6W/m^2 . The highest and lowest O_2 levels observed under NH_4^+ regime was respectively 20.5 % (light flux of 114.7W/m^2) and 17.9% (light flux 147.1W/m^2).

Interestingly, the O_2 levels were found to decrease towards the latter half of NH_4^+ regime (Fig. 5). The O_2 decreased significantly (p value <0.05) from an average of 20% (D11-D15) to 19% over the last five days (D16-D20) of NH_4^+ regime.

3.3 Urea Regime

The transition to urea was performed on D21 of GD. As was done for NH_4^+ transition, the first five days (D21-D25) of NH_4^+ -to-urea transition were not considered for analytical purposes. Consequently, D26-D35 were considered under urea regime.

A total of 1190 readings were recorded under the urea regime. The system maintained average O_2 level of 20.3% over the 10 days of urea regime and applied average light flux of 146W/m^2 (Fig.3 and Fig.6). The system applied the highest possible light flux (147.1W/m^2) on 34.6% of the observed timepoints (412 out of 1190). The highest and lowest reached O_2 levels observed under urea regime were 21.2% (light flux 106W/m^2) and 19.2% (light flux 123.21W/m^2), respectively.

In contrast to the NH_4^+ regime, where the O_2 levels decreased towards the latter half of the NH_4^+ regime, the O_2 levels in fact increased towards the end of urea regime (Fig.3 and Fig.6). While the system reached average O_2 levels of 20% during the first five days (D26-D30) of urea regime, this value increased to 20.4% (p value <0.05) towards the last five days (D31-D35) of urea regime.

3.4 Impact on mouse

At the end of the GD study, the mouse was taken out of the consumer compartment and its health and activities were for one week. The mouse weighed 21.2 gm before the start of study

and it weighed 21.4 gm at the end of the study. There were no visible signs of stress or injury on the body of the mouse and it responded well to stimuli. In general, no behavioral changes were observed in the mouse after the GD test.

4. Discussions

The BIORAT-2 GD lasted for a total of 35 days (in continuous feeding mode). During these 35 days we evaluated (1) the effect of alternative N-sources (NO_3^- , NH_4^+ and urea) on O_2 levels in the gas loop, (b) the possibility to use CO_2 (not monitored) from consumer compartment as C-source for *Limnospira indica* and (c) the efficiency of control law to simulate O_2 production in producer compartment by modulating incident light flux (reaching the PBR) in accordance with the changing of O_2 requirements in the consumer compartment.

The control law used for this study was formulated on the basis of the Photosim 2.0 model described in our previous study (Sachdeva et al., 2018a). The Photosim 2.0 Model is a light-transfer based stochastic model which takes into account the stoichiometric characteristics of the cyanobacterial biomass, cultivation parameters of the bioprocess and geometry of the PBR to predict the volumetric biomass and O_2 productivities. The original Photosim model (Cornet and Dussap, 2009) was developed and validated for *Limnospira indica* PCC 8005 strain (used for this study) cultivated at pH 9.5 with 28 mM NO_3^- (as N-source). Since the nutrient source, its concentration and other cultivation parameters are known to impact the biochemical and stoichiometric content of the photosynthetic species (Sachdeva et al., 2016a and 2016b), we updated the original Photosim model in context of the revised cultivation parameters used for this GD study. Therefore, all the cultivation parameters (dilution rate, residence time, N-feeding concentration, etc.) used to for this GD have also been adapted from our previous study, which was used to validate the Photosim 2.0.

The Photosim 2.0 model was only updated to be used for NO_3^- and NH_4^+ (as N-sources) feeding conditions. Accordingly, the control law used for this GD study was optimized for NO_3^- and NH_4^+ feeding conditions and not for urea. Regardless we decided to include urea as one of the N-sources for this study mainly because of two reasons. Firstly, urea is one of the main components of non-nitrified (untreated) urine (Chang et al., 2013) and if untreated/partially treated urine is to be used as N-source for cyanobacterial cultivation, it is important to test the effect of urea on O_2 production capacity of *Limnospira indica*. Secondly, our previous studies (Deschoenmaeker et al., 2017; Sachdeva et al., 2018b) have indicated that *Limnospira* sp. have better tolerance for urea (vs NH_4^+), so it was important to compare the O_2 production capacity of *Limnospira indica* under all three N-source in the same experiment. Interestingly, the control law performed exceptionally well for urea regime.

It is also important to note here that attaining “gas-steady-state”, was used for defining the steady-state criteria for this GD study. This was in contrast to most bioprocess studies, which normally focus on attaining use “liquid-steady state”. The gas-steady-state criteria was mainly based on the objective of this GD study, which aimed to evaluate the effect of alternative N-sources on the O_2 production capacity of *Limnospira indica*. In order to attain “liquid-steady-state”, the system must be maintained under continuous feeding of a particular N-source for a minimum of three residence times (15 days), which would have considerably increased the overall duration of the GD study. On other hand, the constraints linked with maintenance of the mouse in the consumer compartment for longer than 40 days (cage hygiene, animal stress) and ethical guidelines for the animal experimentation did not permit us to conduct such long duration experiments. Therefore, we focused on attaining “gas-steady state” (two residence times) for the purpose of this GD study.

Another important consideration for this GD study was the exclusion of first five days of N-source transition (NO_3^- to NH_4^+ and NH_4^+ to urea) from quantitative analysis. This criterion

was also defined on the basis of our previous study (Sachdeva et al., 2018a), wherein we observed that the Photosim 2.0 model worked best for the timepoints wherein the PBR was under a single N-source (with 80% fitting between experimental and simulated values). The prediction efficiency of the model reduced (to 50% fitting between experimental and simulated values) when the PBR was undergoing a transition between two N-sources. In other words, Photosim 2.0 model prediction were found to be less efficient when two N-sources were simultaneously present in the PBR. Based on these results we decided to exclude the first five days of NO_3^- to NH_4^+ transition (D6-D10) and NH_4^+ to urea transition (D21-D25) from our quantitative analysis (Fig.S1). The effect of simultaneous presence of multiple N-sources on the volumetric productivity of the PBR are currently being studied by our group in order to be able to more accurately describe the effect of N-transition.

Overall, the system maintained average O_2 levels of 20.3% during the NO_3^- regime and applied average light flux of 136W/m^2 (Fig.3). Overall, the O_2 levels were found to be quite stable under NO_3^- regime compared to NH_4^+ and Urea regime (Fig.3 and Fig.S1). We did observe some fluctuations in the individual O_2 readings (after averaging). But these variations were due to the perturbation of the electrochemical O_2 sensor (used for this study) due to the high gas flow rates in the sensor line. For more accurate measurements, highly accurate sensors like the ones that work on the principle of paramagnetic-susceptibility of O_2 should be used for the future studies.

The system was constantly working under the maximum light flux of 147.1W/m^2 (possible with the light unit used for this GD study) for most part of NH_4^+ regime (83% of observed timepoints). The system reached average O_2 levels of 19.5% under NH_4^+ regime, by applying average light flux of 146.6W/m^2 (Fig. 3). Interestingly, the average O_2 levels further decreased during the latter half of NH_4^+ regime. The lower O_2 levels observed under NH_4^+ regime (vs NO_3^- regime) were in accordance with the results of our previous study (Sachdeva et al.,

2018a), wherein we had reported 21.5% decrease in O₂ yields under NH₄⁺ regime (vs NO₃⁻ regime). A brief simulation summary comparing the RO₂ (oxygen production rate, mMO₂/L/hr) of *Limnospira indica* cultivated at different light flux (q₀) under NO₃⁻ and NH₄⁺ regimes, has been described under Appendix 1. Appendix 1 summarizes the RO₂ for both NO₃⁻ and NH₄⁺ regimes as the function of light flux (q₀; W/m²) and biomass concentration (g/L) (Fig.A1, Appendix 1). Finally, a comparison has been made between the (difference of) RO₂ for NO₃⁻ and NH₄⁺ regimes at different biomass concentrations (g/L) at the applied light flux of 146W/m² (Fig.A2, Appendix 1). This simulation data also suggests that at the desired biomass concentration of 2.0 g/L (used for validation of Photosim Model 2.0) and applied light flux of 146W/m², 20% lower RO₂ is expected under NH₄⁺ regime (vs NO₃⁻ regime).

Evidently, the system would have to produce 121% higher O₂ under NH₄⁺ regime to compensate for the 21.5% lower O₂ yields (vs NO₃⁻ regime). This theoretically means that higher light flux of 155.8W/m² would be needed to reach the desired setpoint 20.3% O₂ under NH₄⁺ regime. This could only be achieved by increasing the photosynthetic efficiency in the producer compartment, since the nutrient concentration, feeding rate and other cultivation parameter could not be altered (as per study protocol). Moreover, the rate of photosynthesis was not foreseen to be limited by CO₂ levels under the present working conditions. This is mainly because under the cultivation parameters (biomass concentration, dilution rate, O₂ yield and light flux) used for this GD study, the product of respiration quotient and photosynthetic quotient was approximately 1.2 (see Demey et al., 2000 for details). This means that the rate of production of O₂ is more than the rate of consumption of CO₂. Hence the lower O₂ levels observed under the NH₄⁺ regime could only be improved by increasing the incident light flux. However, due to the limitation of the hardware used in this GD, it was practically impossible to attain this level of light flux. For the future LSS studies (especially where NH₄⁺ is used as the N-source), it would be important to evaluate the possibility of using higher light flux to

enhance the photosynthetic efficiency (and hence O₂ production capacity) of *Limnospira* without subjecting the cells to photo-inhibition. Such an investigation becomes even more important in context of LSS studies wherein the cyanobacterial biomass is intended to be used as a nutrition source for the crew. Since light stress is known to change the biochemical composition of cyanobacterial biomass and reduce its nutrient content (Chentir et al., 2018), extensive research needs to be undertaken to derive the ideal working light intensities that can increase the O₂ yield of *Limnospira* culture fed with NH₄⁺ without subjecting it to photo-inhibition or compromising on the nutrient content of the biomass.

We also observed considerable amount of biofilm deposition in PBR and cyanobacterial cell bleaching (from bright green to pale-green) under NH₄⁺ feeding (data not shown), which increased towards the latter half of NH₄⁺ regime. The decreased O₂ levels and increased biofilm deposition in the PBR clearly indicated that the cyanobacterial cells were under nutrient stress (Rossi and De Philippis, 2015), indicating that NH₄⁺ would not be able to meet the metabolic needs of *Limnospira*. Based on these results we can say, that in order to avoid these inhibitions (in terms of lower O₂ levels and nutrient stress) either the NH₄⁺ only N-regimes would need to be limited to shorter durations or NH₄⁺ would have to be combined with other N-sources to overcome this inhibition. Consequently, it would be interesting to analyze the effect of mix/combination of NH₄⁺ with other N sources on the metabolic characteristics and oxygen production capacity of *Limnospira indica* through future studies.

In contrast to the NH₄⁺ regime, the system could effectively reach the desired (setpoint) O₂ levels of 20.3% under urea regime (Fig.6). Though comparable (average) O₂ levels were observed under urea and NO₃⁻ regime, the system had to apply under higher light flux to reach these levels under urea regime (average light flux 146W/m²). But it is important to reiterate here that the control law and Photosim 2.0 model had not been previously validated of urea feeding conditions. The light-transfer parameters used to validate the Photosim 2.0 model (and

hence the control law) are influenced by the nutrient source, its effect on stoichiometry of cyanobacterial biomass and the resulting light-transfer/ absorption coefficients (Cornet et al., 1992 and 1995; Cornet and Dussap, 2009). Consequently, these prediction parameters are expected to change under urea feeding conditions.

Even though, the system worked under light saturation for both NH_4^+ and urea regimes, it could maintain 20.3% O_2 level under urea regime. This indicated that urea is a better N-source (vs NH_4^+) for supporting the photosynthetic needs of *Limnospira indica*. Moreover, contrary to the NH_4^+ regime, where the O_2 levels decreased during the last five days of NH_4^+ feeding, the O_2 levels slightly increased during the latter half of urea regime (Fig.3). The higher O_2 levels under urea regime could be attributed to its stoichiometry. Urea metabolism produces 2- NH_4^+ and CO_2 . The influx of additional CO_2 (from urea metabolism) might have supported photosynthesis (and hence O_2 production). Higher N and carbon availability under urea regime could be the reason for the revival of cells (from nutrient stress). This was also evident from the decreased biofilm deposition in the PBR once the urea feeding was started. The biofilm formation and cell bleaching observed during the NH_4^+ regime, started to decrease with urea feeding and disappeared by the second half of urea regime (data not shown). These physical indicators further showed that compared to NH_4^+ , urea is a better N-source (both stoichiometrically and bio-energetically) for meeting the metabolic needs of *Limnospira indica* (Sassano et al., 2004).

5. Conclusion and Future Perspectives

This GD study, broadened our knowledge and understanding about the possibility of using different N-sources present in non-nitrified urine for cyanobacterial cultivation and air-revitalization. In our previous batch and continuous feeding studies we have already evaluated the effect of the different N-sources and their varying concentrations on the yield and biochemical content (carbohydrates, lipids, proteins, phycobiliproteins and chlorophyll) of

Limnospira biomass (Deschoenmaeker et al., 2017; Sachdeva et al., 2018a and 2018b). Since NH_4^+ and urea are the main N-sources present in non-nitrified urine (Chang et al., 2013), it was important to test the effect of these N-sources on the O_2 production capacity of *Limnospira indica* compared to NO_3^- (the main component of nitrified urine).

In summary, we found that the system could easily maintain the ambient O_2 levels of 20.3 % under NO_3^- and urea regime, indicating that *Limnospira indica* PCC 8005 adapted better to urea over ammonium under comparable cultivation conditions.

However, it would be necessary to validate the Photosim model for urea feeding conditions. This could also help to improve the control law for urea feeding conditions. This understanding would be even more important when the tests/ experiments would be conducted in the actual setup of the MELiSSA LSS. For the present study, we used a modified version of MELiSSA loop, wherein we had closed loop for the “gas-phase” of the system, but the system was open (not fully closed) on the liquid side and thus CO_2 accumulation was not anticipated. However, under the actual MELiSSA loop setup, attaining O_2/CO_2 equilibria would be even more complex due to the involvement of several other compartments (see Fig.1A). In such a scenario we will have to focus on attaining carbon-balance and not just CO_2 balance.

Furthermore, it would be important to investigate the effect of mix of N-sources on cyanobacterial cultivation and air-revitalization, mainly for future LSS studies, wherein fluctuating streams of partially treated urine are planned to be used as N-source for cyanobacterial cultivation.

More importantly, it would also be interesting to investigate the cumulative effect of different N-sources, high urine salinity, different organic compounds (metabolites, hormones, amino acids, etc.) and other personal hygiene products present in human urine, on the overall metabolism, stoichiometry and O_2 production capacity of *Limnospira indica*. These

experiments become even more important for regenerative LSS studies, mainly because influx of external carbon-sources in from organic compounds (present in urine) will not only change the cultivation mode from photoautotrophic to mixotrophic regime but would also have an effect on the biochemical/ nutrient content of the biomass. In this regards we are conducting further studies to evaluate the effect of simultaneous presence of different N-sources, organic compounds and high urine salinity mixture of different N-sources on the biomass and oxygen productivities of *Limnospira indica*. The biochemical data obtained from these ongoing studies will be used to optimize the prediction parameters of Photosim model which will then be used to perform future GD studies.

In conclusion, this GD study provided preliminary indications towards the possibility of using NH_4^+ and urea rich medium and CO_2 from consumer compartment for *Limnospira indica* cultivation and air-revitalization. The cumulative conclusions from our previous, present and upcoming studies would not only aid in designing more efficient and robust regenerative life support systems for future space missions but would also help in gaining better understanding towards the design of economically viable microalgae-based waste-water remediation systems and photosynthetic biorefineries for terrestrial purposes.

Data Availability Statement

The supplementary data can be found in the online version of this paper.

Author Contributions

NS conducted all the experiments the data. NS and LP worked on the Photosim 2.0 model. BL and OG worked on the control law. CGD, CL, BL and RW supervised the study. NS wrote the manuscript. All authors contributed equally to data analysis, interpretation and manuscript review.

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Figure Captions

Fig.1A: A schematic of Micro Ecological Life Support System Alternative (MELiSSA) loop.

Fig. 1B: A schematic of the breadboard layout used for ground demonstration study.

PBR unit: Photobioreactor plus the lightening unit; **PI:** Pressure monitor; **FT:** Flow transmitter; **FC:** Flow controller; **CC:** Consumer compartment; **O₂:** Oxygen sensor.

Fig.2: A schematic of the timelines and study protocol adopted for the ground demonstration study.

Fig.3: A comparative of the average oxygen (% O₂) and light flux (W/m²) values quantified during the three nitrogen regimes of ground demonstration study. *For the graphical representation of data, the values have been reported as the 15 minutes average of each analyte.*

Fig.4: A comparative of the average oxygen (% O₂) and light flux (W/m²) values quantified by the monitoring system during the nitrate regime (Day 1- Day 5). *For the graphical representation of data, the values have been reported as the 15 minutes average of each analyte.*

Fig.5: A comparative of the average oxygen (% O₂) and light flux (W/m²) values quantified by the monitoring system during the ammonium regime of ground demonstration (Day11- Day 20). *For the graphical representation of data, the values have been reported as the 15 minutes average of each analyte.*

Fig.6: A comparative of the average oxygen (% O₂) and light flux (W/m²) values obtained during the urea regime of ground demonstration (Day 26- Day 33). *For the graphical representation of data, the values have been reported as the 15 minutes average of each analyte.*

Figure 1.JPEG

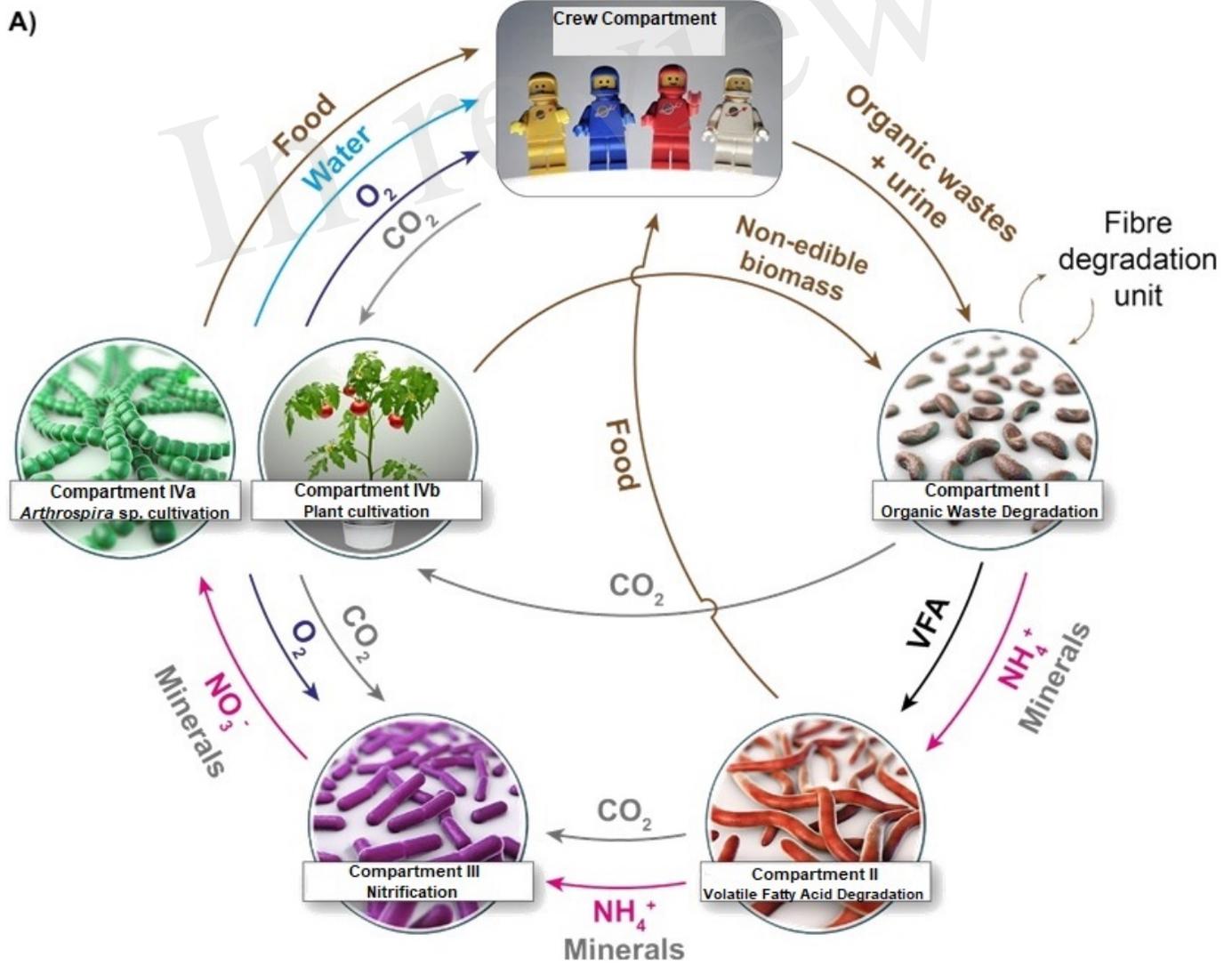


Figure 2.JPEG

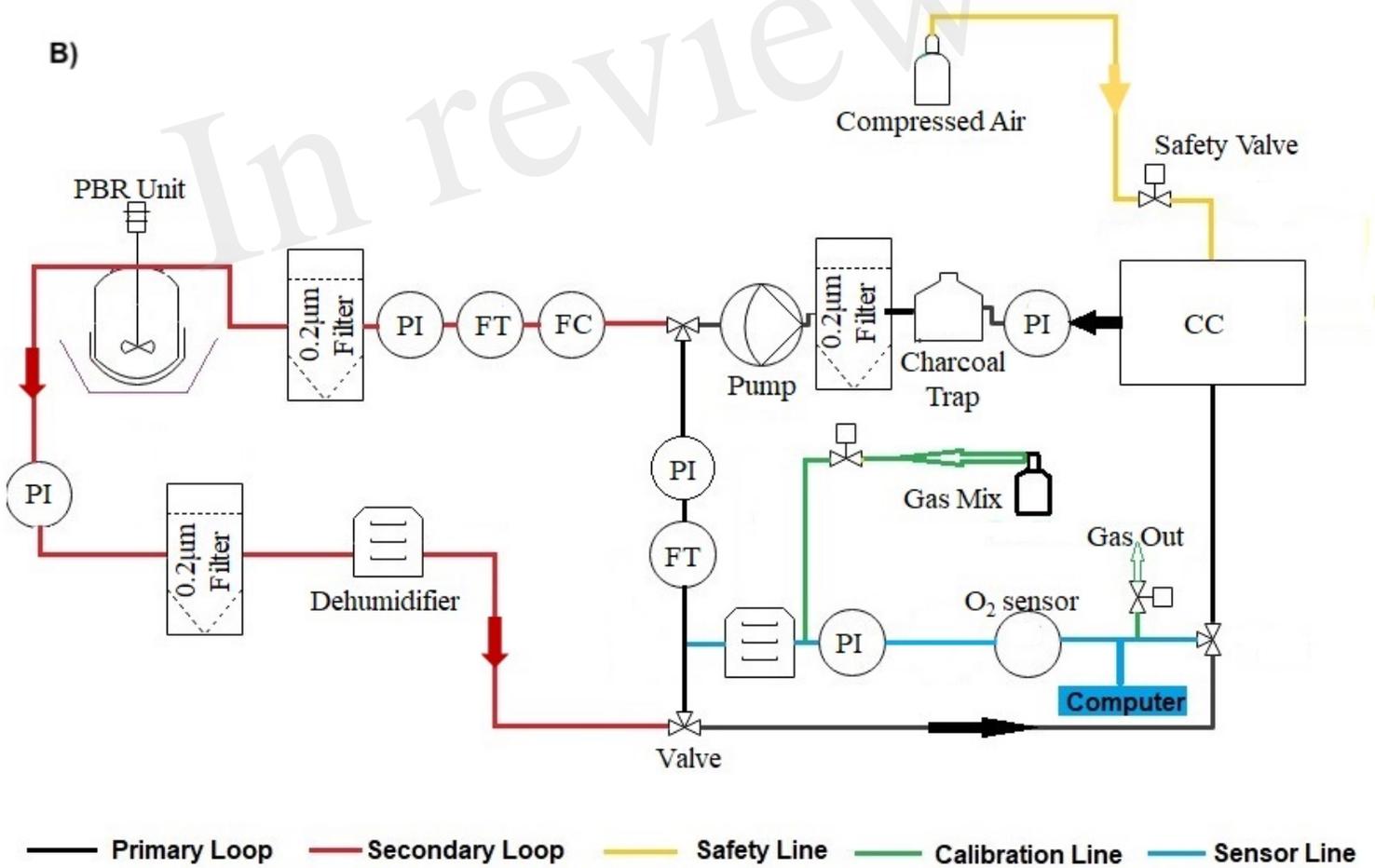


Figure 3.JPEG

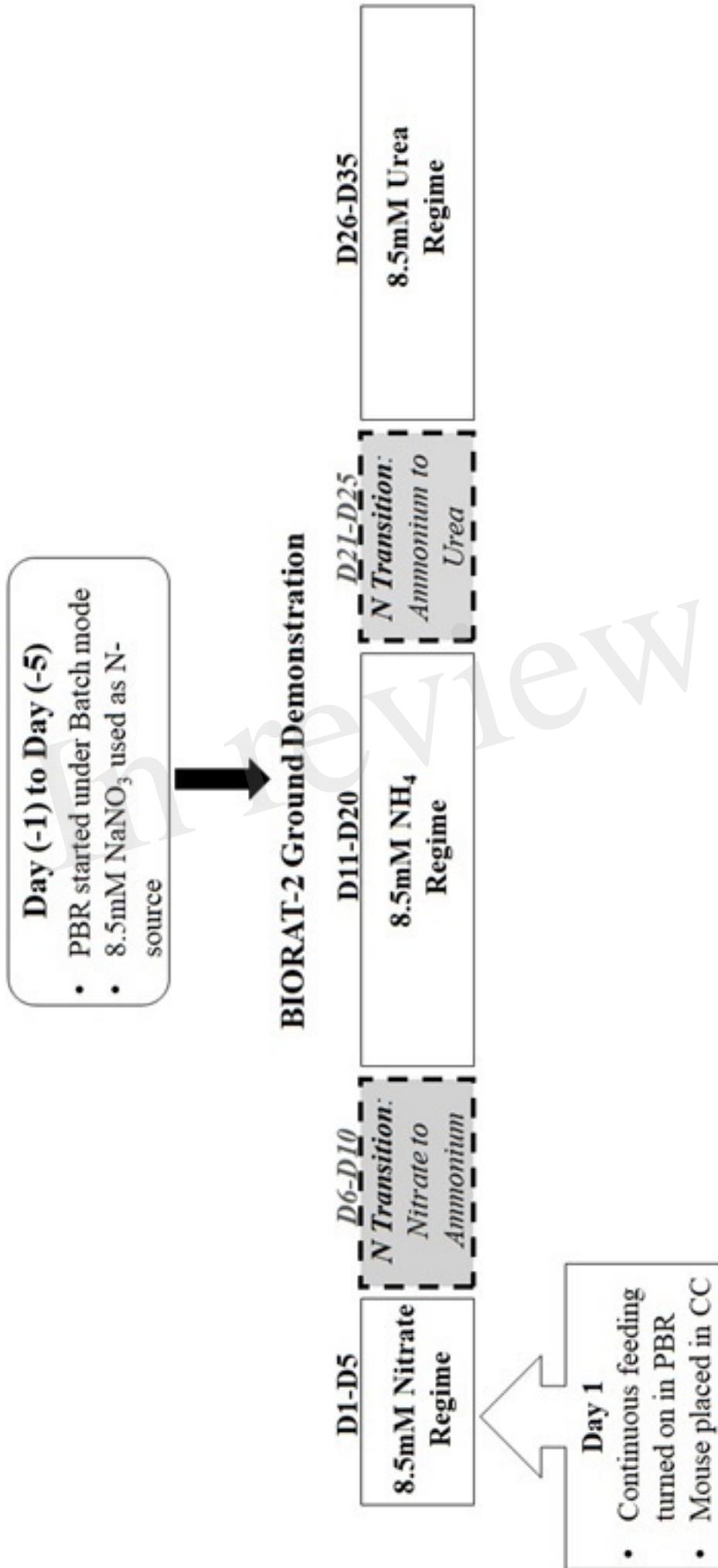
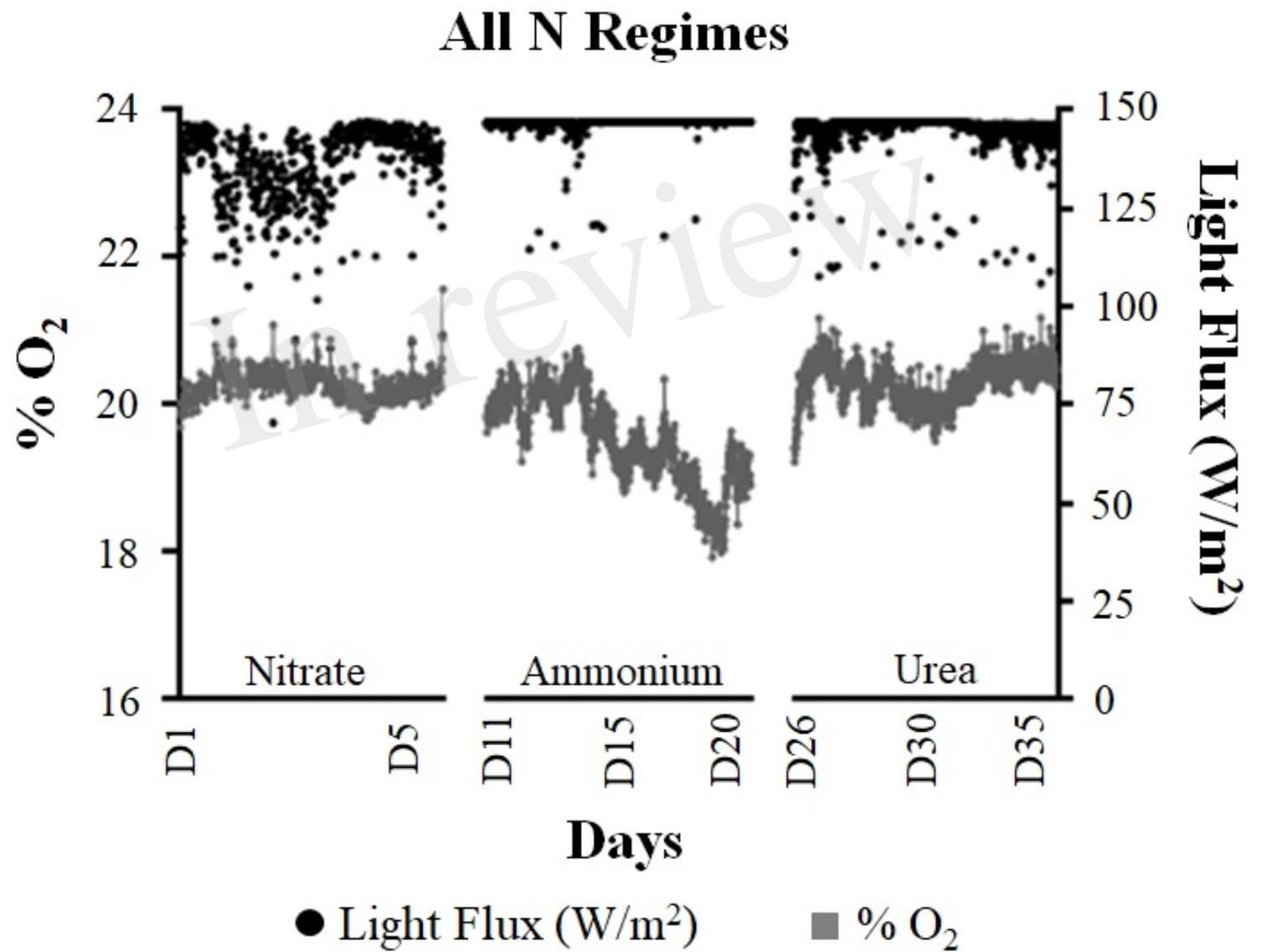
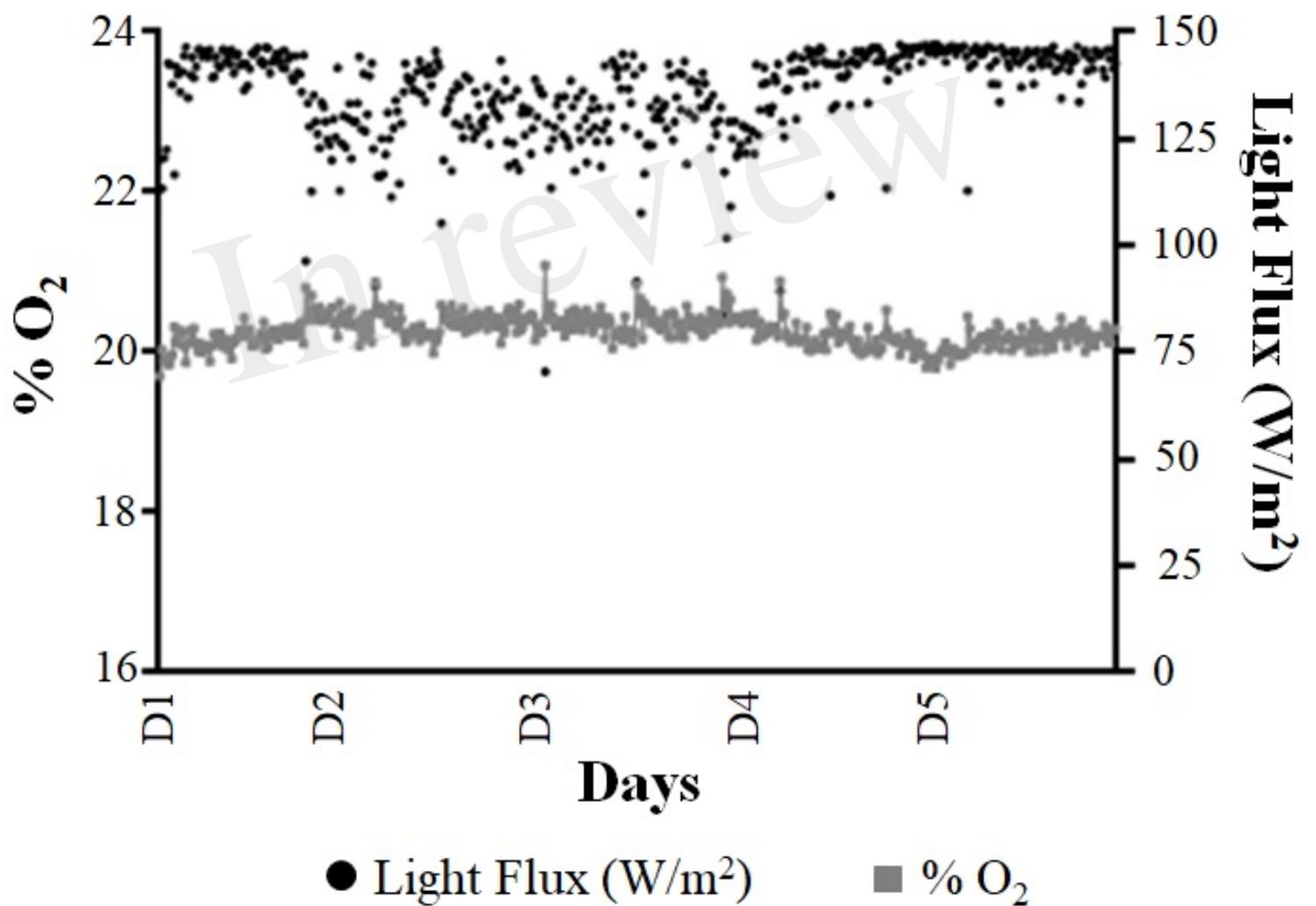


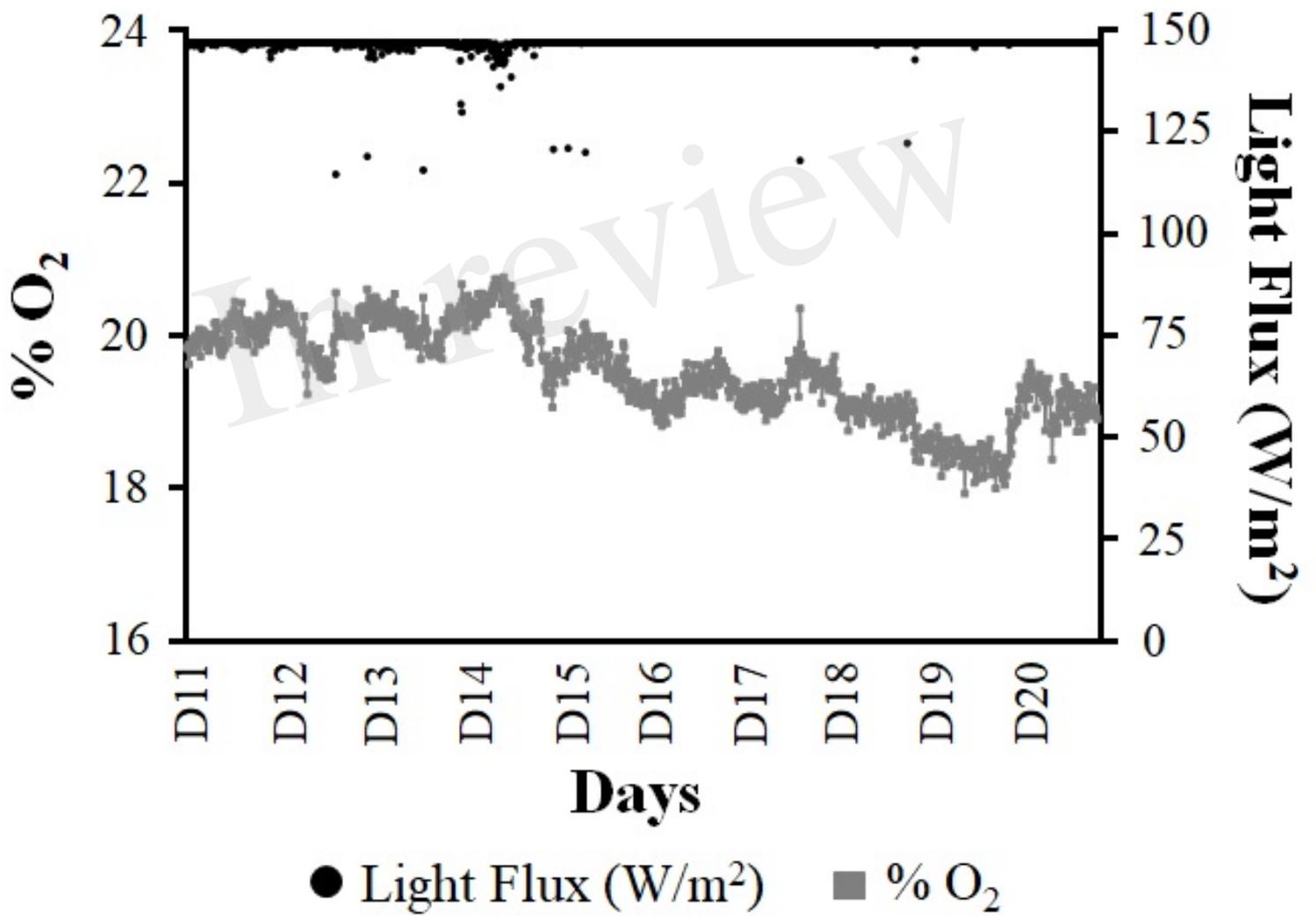
Figure 4.JPEG



Nitrate Regime (D1-D5)



Ammonium Regime (D11-D20)



Urea Regime (D26-D35)

